





Adaptation of the Lagrangian module of a CFD code for atmospheric dispersion of pollutants in complex urban geometries and comparison with existing Eulerian results

> Meissam Bahlali, E. Dupont, B. Carissimo CEREA – EDF R&D, Chatou, France



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## **1.** CONTEXT AND OBJECTIVES

2. HOW TO MODEL ATMOSPHERIC DISPERSION?

**3.** LAGRANGIAN STOCHASTIC MODELS

4. VALIDATION CASE: CONTINUOUS POINT RELEASE WITH UNIFORM MEAN SPEED AND TURBULENT DIFFUSIVITY





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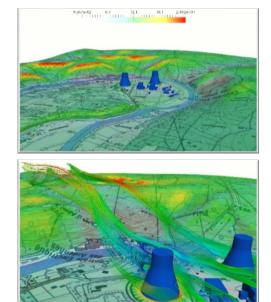


# CONTEXT AND OBJECTIVES

Source: R. Bresson, EDF R&D

### Context:

- Turbulent dispersion = advection + turbulent diffusion.
  - wide range of eddies in the atmospheric boundary layer which all participate in their own way to the transport and diffusion of the cloud
  - in particular: turbulent dispersion is not as effective close to the emission source as opposed to further away → need to correctly model the effect of the different turbulent structures.
- Multiple families of models: Gaussian, Eulerian (SGDH, GGDH, AFM, DFM...), Lagrangian models...



### Objectives:

- To adapt of the Lagrangian stochastic model of the CFD code Code\_Saturne in order to simulate near-field dispersion of pollutants in complex environments including buildings and taking into account atmospheric stratification.
- □ To complete the existing Eulerian modelling of these phenomena → compare and clarify the differences between the approaches, making use of the same CFD code.







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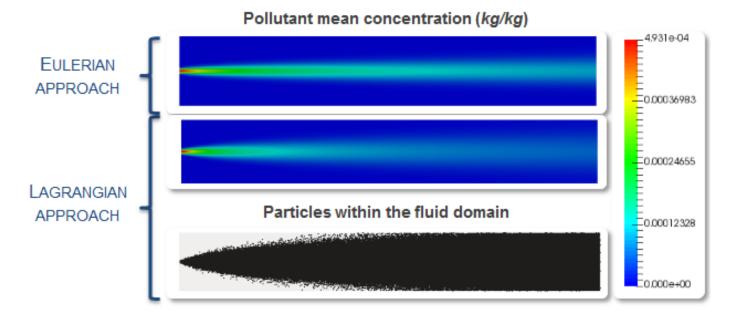
## PRESENTATION OF THE APPROACH

• Calculation of the flow field ("continuous phase"): mean Navier-Stokes equations

$$\begin{cases} \frac{\partial \bar{\rho}}{\partial t} + \frac{\partial (\bar{\rho} \widetilde{u}_i)}{\partial t} = 0\\ \frac{\partial (\bar{\rho} \widetilde{u}_i)}{\partial t} + \frac{\partial (\bar{\rho} \widetilde{u}_i \widetilde{u}_j)}{\partial x_j} = -\frac{\partial \bar{p}}{\partial x_i} + \frac{\partial}{\partial x_i} (\overline{\tau_{ij}} - \bar{\rho} \overline{u'_i u'_j}) - \bar{\rho} g \delta_{iz} \end{cases}$$

- Calculation of the dispersion of the pollutants within this flow field (*"dispersed phase"*): 2 main types of models
  - Eulerian/Eulerian models
  - Eulerian/Lagrangian models

## EULERIAN AND LAGRANGIAN APPROACHES



## EULERIAN APPROACH

Mean advection-diffusion equation for a scalar c:

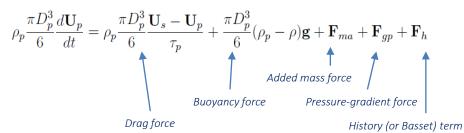
$$\frac{\partial \bar{c}}{\partial t} + \bar{u}_j \frac{\partial \bar{c}}{\partial x_j} = \frac{\partial}{\partial x_j} \left( D \frac{\partial \bar{c}}{\partial x_j} - \overline{u'_j c} \right) + \bar{S} + \bar{R}$$

Velocity and turbulence fields → solved by the CFD code
 Code\_Saturne using RANS models with classical k-ε or R<sub>ij</sub>-ε closures adapted to the atmosphere and complex geometries

#### $\rightarrow$ APPROACH THAT HAS BEEN USED AT EDF R&D SO FAR.

## LAGRANGIAN APPROACH

Particle's equation of motion:



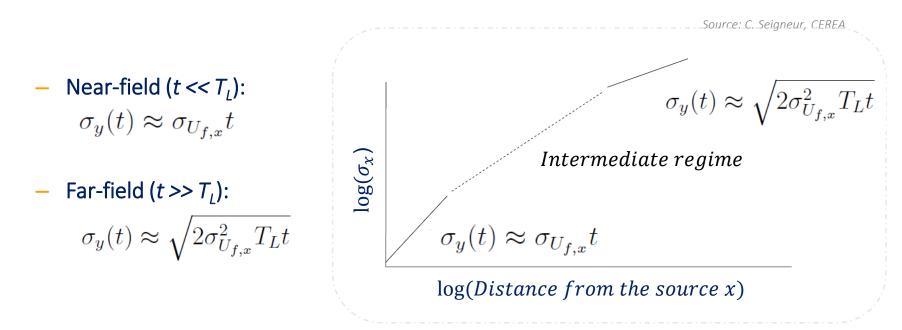
where:  $U_s(t) = U_f(X(t),t)$  is the velocity of the fluid sampled through the trajectory of the particle

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## WHY USE A LAGRANGIAN MODEL?

• **Diffusion theory** [Taylor, 1921] → if we consider particle dispersion from a point source in stationary isotropic turbulence, there are 2 different regimes of diffusion:

$$\sigma_y^2(t) = 2\sigma_{U_{f,x}}^2 \int_0^t (t-s) R_{L,x}(s) \,\mathrm{d}s$$



## WHY USE A LAGRANGIAN MODEL?

• Eulerian approach used at EDF R&D so far: RANS with *k-e* closure. However: turbulent viscosity models imply a turbulent diffusivity *K* independent from the distance to the source and:

$$\sigma_y(t) = \sqrt{2Kt}$$
 where:  $K = C_\mu \frac{k^2}{\epsilon}$   $\propto \sqrt{t}$ 

→ This model is unable to reproduce near-field behaviour.

• Lagrangian approach with Langevin model yields [Pope, 2001]:

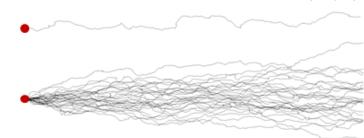
$$R_L(s) = exp(-|s|/T_L)$$

hence:

$$\sigma_y^2(t) = 2\sigma_{U_{f,x}}^2 T_L[t - T_L(1 - e^{-t/T_L})] \xrightarrow[t \to T_L]{t \to T_L} \sigma_y(t) \approx \sigma_{U_{f,x}} t$$

→ This model does discriminate the two different diffusion regimes. Note that: an Eulerian RANS model not based on turbulent viscosity approx. but with a complete transport of turbulent scalar fluxes ("DFM") would also have this property → work in progress.





Source: RECORD report (ECL)

• Equation of motion solved for each particle:

Particles' displacement within a turbulent flow

$$\rho_p \frac{\pi D_p^3}{6} \frac{d\mathbf{U}_p}{dt} = \rho_p \frac{\pi D_p^3}{6} \frac{\mathbf{U}_s - \mathbf{U}_p}{\tau_p} + \frac{\pi D_p^3}{6} (\rho_p - \rho) \mathbf{g} + \mathbf{F}_{ma} + \mathbf{F}_{gp} + \mathbf{F}_h$$

where:  $U_s(t) = U_f(X(t), t)$  is the velocity of the fluid sampled through the trajectory of the particle

- → This equation needs closure. Indeed:  $\mathbf{U}_{s}(t) = \mathbf{U}_{f}(\mathbf{X}(t), t) = ?$
- Code\_Saturne with RANS models only provides:  $\langle \mathbf{U}_{f}(\mathbf{X}(t),t) \rangle$

## → PDF (PROBABILITY DENSITY FUNCTION) METHODS:

development of a Lagrangian stochastic model to reconstruct the turbulence effects



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# MODEL FOR U<sub>s</sub>: *SIMPLE LANGEVIN MODEL* [POPE, 2001]

Where: 
$$T_{L,i}^* = \frac{T_{L,i}}{1 + \beta \frac{|\mathbf{U}_f - \mathbf{U}_p|}{\sqrt{\frac{2}{3}k}}}$$
 and  $\beta = \frac{T_{L,i}}{T_{E,i}}$  and  $T_{L,i} = \frac{1}{\frac{1}{2} + \frac{3}{4}C_0} \frac{k}{\epsilon}$ 

# MODEL FOR U<sub>s</sub>: OTHER MODELS...

- Let us consider, for the sake of simplicity, the case of fluid particles:  $\mathbf{U}_s = \mathbf{U}_p$
- 2 ways of modelling the evolution of the velocity field:
  - Through the instantaneous velocity  $\mathbf{U}_{p}$
  - Through the fluctuating velocity  $\mathbf{U}_{p}' = \mathbf{U}_{p} \langle \mathbf{U}_{f} \rangle \Rightarrow d\mathbf{U}_{p}' = d\mathbf{U}_{p} d \langle \mathbf{U}_{f} \rangle$

Model using:	Formulation
Instantateous velocity	$dU_{p,i} = -\frac{1}{\rho} \frac{\partial \overline{P}}{\partial x_i} dt - \frac{U'_{p,i}}{T_{L,i}} dt + \sqrt{C_0 \overline{\epsilon}} dW_i$
Fluctuating velocity	$dU'_{p,i} = \left(\frac{\partial \overline{U'_{f,i}U'_{f,j}}}{\partial x_j} - U'_{p,j}\frac{\partial \overline{U_{f,i}}}{\partial x_j}\right)dt - \frac{U'_{p,i}}{T_{L,i}}dt + \sqrt{C_0\overline{\epsilon}}dW_i$

[Minier, Chibbaro, Pope, 2014]

Obtained using

Navier-Stokes eq.

# MODEL FOR U<sub>s</sub>: OTHER MODELS...

Model using:FormulationInstantateous velocity $dU_{p,i} = -\frac{1}{\rho} \frac{\partial \overline{P}}{\partial x_i} dt - \frac{U'_{p,i}}{T_{L,i}} dt + \sqrt{C_0 \overline{\epsilon}} dW_i$ Fluctuating velocity $dU'_{p,i} = \left(\frac{\partial \overline{U'_{f,i}U'_{f,j}}}{\partial x_j} - U'_{p,j} \frac{\partial \overline{U_{f,i}}}{\partial x_j}\right) dt - \frac{U'_{p,i}}{T_{L,i}} dt + \sqrt{C_0 \overline{\epsilon}} dW_i$ 

• Example: [Thomson, 1987] model  $\rightarrow$   $dU'_{p,i} = a_i dt + b_{ij} dW_i$  where:

$$a_{i} = -\frac{C_{0}\epsilon}{2}\delta_{ij}\Gamma_{jk}U'_{p,k} + \frac{\Phi_{i}}{g_{a}} \qquad \text{and} \quad \frac{\Phi_{i}}{g_{a}} = \overline{U_{f,l}}\frac{\partial\overline{U_{f,i}}}{\partial x_{l}} + \frac{\partial\overline{U_{f,i}}}{\partial x_{j}}(U_{p,j} - \overline{U_{f,j}}) + \qquad - \begin{array}{c} \text{Gaussian turbulence hypothesis} \\ - \begin{array}{c} \text{Complicated formulation} \\ \frac{1}{2}\frac{\partial\tau_{il}}{\partial x_{l}} + \frac{1}{2}\overline{U_{f,m}}\frac{\partial\tau_{il}}{\partial x_{m}}\Gamma_{lj}(U_{p,j} - \overline{U_{f,j}}) + \\ & \\ \frac{1}{2}\frac{\partial\tau_{il}}{\partial x_{k}}\Gamma_{lj}(U_{p,j} - \overline{U_{f,j}})(U_{p,k} - \overline{U_{f,k}}) \end{array}$$

- Instantateous velocity: pressure-gradient term clearly visible
- *Fluctuating velocity:* term hidden behind (

$$\left(\frac{\partial \overline{U'_{f,i}U'_{f,j}}}{\partial x_j} - U'_{p,j}\frac{\partial \overline{U_{f,i}}}{\partial x_j}\right) dt$$

# MODEL FOR U<sub>s</sub>: OTHER MODELS...

# WHY ARE WE CONCERNED ABOUT THE PRESENCE OF THE PRESSURE-GRADIENT TERM IN OUR MODELS?

- Well-mixed condition problem: *an initially uniform particle concentration in a turbulent flow should remain uniform* 
  - → condition that any Lagrangian stochastic model needs to meet
  - → consistency with the mean Navier-Stokes equations
- [Minier, Chibbaro, Pope, 2014] : if the pressure-gradient term does not appear in the formulation of the model, then the well-mixed condition may not be fulfilled
- Note: need of full pressure field.

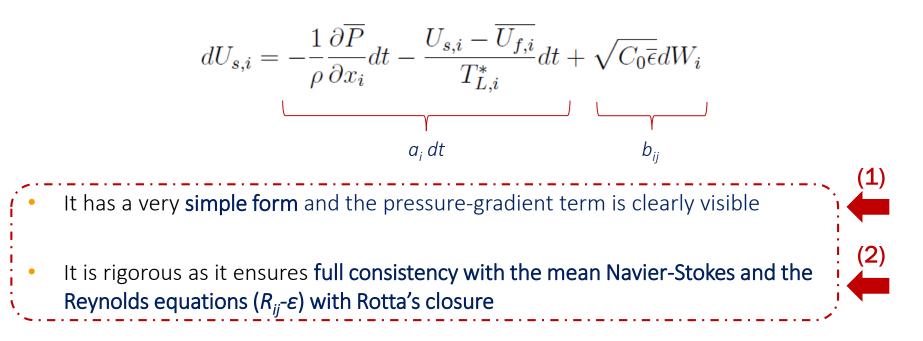
OUR REASONS FOR GOING FURTHER WITH THE SIMPLE LANGEVIN MODEL OF [POPE, 2001]

$$dU_{s,i} = -\frac{1}{\rho} \frac{\partial \overline{P}}{\partial x_i} dt - \frac{U_{s,i} - \overline{U_{f,i}}}{T_{L,i}^*} dt + \sqrt{C_0 \overline{\epsilon}} dW_i$$

$$a_i dt \qquad b_{ij}$$

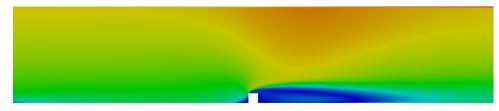
- It has a very **simple form** and the pressure-gradient term is clearly visible
- It is rigorous as it ensures full consistency with the mean Navier-Stokes and the Reynolds equations  $(R_{ij}-\varepsilon)$  with Rotta's closure
- No hypothesis is made on the PDF of the velocity of the particles
- To our knowledge, it has not previously been used in the context of atmospheric dispersion

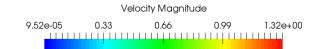
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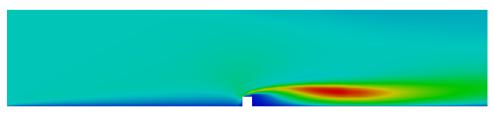


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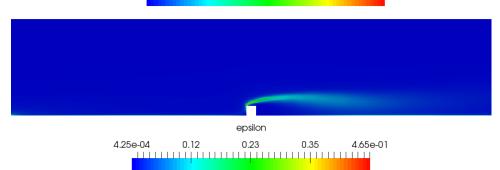
Inhomogeneous turbulence: obstacle within a boundary layer





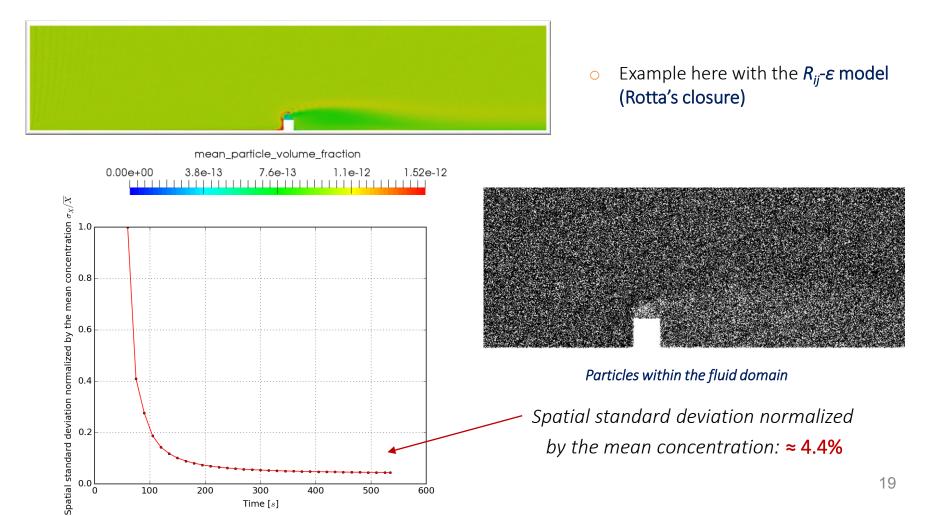


k\_Rij 8.07e-04 0.016 0.031 0.046 6.07e-02



EULERIAN FLOW FIELD

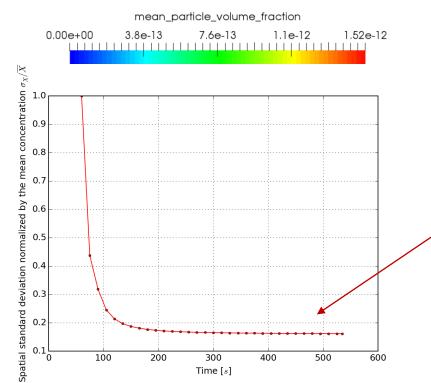
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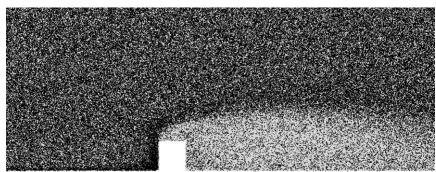


(1) What happens if we do not take into account the pressure-gradient term?



$$dU_{s,i} = -\frac{1}{\rho} \frac{\partial \overline{P}}{\partial x_i} dt - \frac{U_{s,i} - \overline{U_{f,i}}}{T_{L,i}^*} dt + \sqrt{C_0 \overline{\epsilon}} dW_0$$



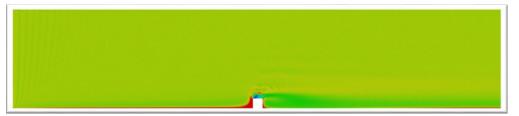


Particles within the fluid domain

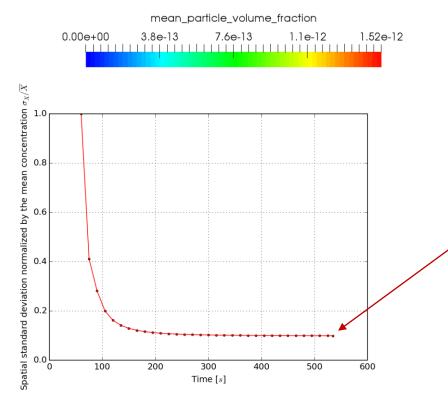
Spatial standard deviation normalized by the mean concentration: ≈ 16.2% > 4.4%! ACCUMULATION OF PARTICLES

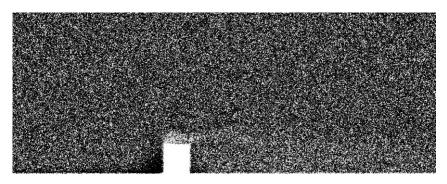
→ SHOWS THE IMPORTANCE OF THE PRESSURE-GRADIENT TERM IN THE LANGEVIN EQUATION

(2) What happens if the turbulence model used for the flow is not consistent with the SLM?



- Model fully consistent with the SLM: *R<sub>ij</sub>-ε* model with Rotta's closure
- Example here with the k- ε model





Particles within the fluid domain

Spatial standard deviation normalized by the mean concentration: ≈ 9.9% >> 4.4%! ACCUMULATION OF PARTICLES

→ SHOWS THE IMPORTANCE OF MODELLING THE FLOW WITH A R<sub>IJ</sub>-EPS MODEL (ROTTA'S CLOSURE)



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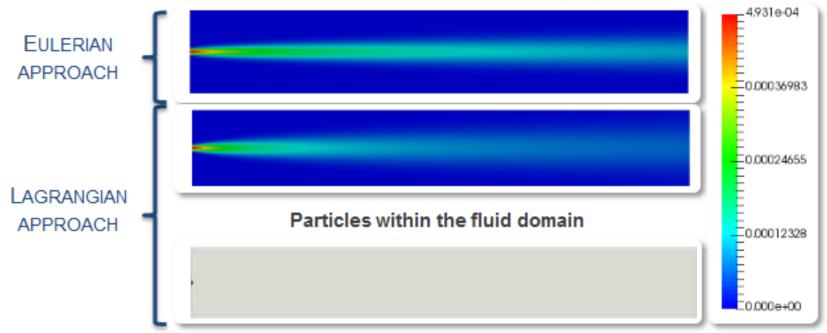


## CALCULATION OF THE DISPERSED PHASE

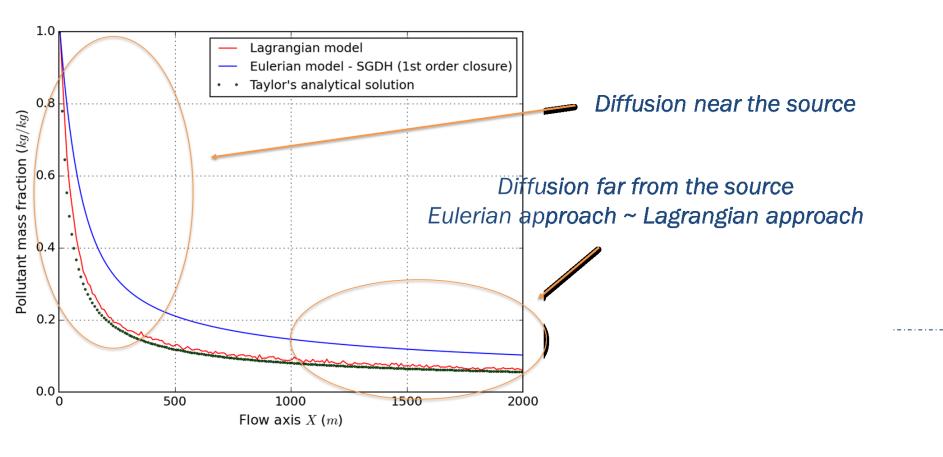
## Taylor's analytical solution:

$$\frac{c}{Q} = \frac{1}{\sqrt{2\pi}U\sigma_x} \text{ with: } \sigma_x = \sqrt{\frac{2}{3}k} \frac{x}{U\sqrt{1+\frac{x}{2UT_L}}}$$

### Pollutant mean concentration (kg/kg)



## CALCULATION OF THE DISPERSED PHASE



Maximum concentration (kg/kg) along the flow axis Comparison of the two approaches

# CONCLUSIONS AND PERSPECTIVES

Conclusions:

 Objective: development of a Lagrangian stochastic tool to simulate atmospheric dispersion simultaneously with Eulerian dispersion

□ *Simple Langevin Model* of [Pope, 2001] : to our knowledge, never used in the context of atmospheric dispersion  $\rightarrow$  yet, many advantages:

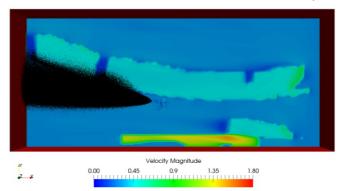
- Pressure-gradient term included in an evident manner  $\rightarrow$  *no spurious drifts*
- Full consistency with the  $R_{ij}$ -eps model (Rotta's closure)  $\rightarrow$  careful when calculating the continuous phase!
- Validation of the well-mixed criterion: our model performs well, even with an obstacle within a boundary layer
- Validation by checking with analytical solution: with our Lagrangian model, distinction of the two regimes of diffusion

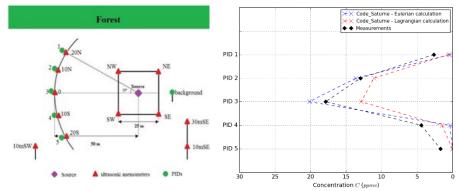


# **CONCLUSIONS AND PERSPECTIVES**

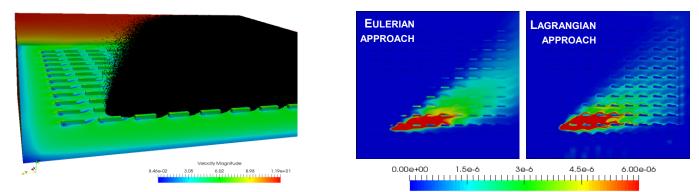
### Perspectives:

**validation** on SIRTA campaign with  $R_{ij}$ - $\varepsilon$  model (consistency issues between Navier-Stokes/Langevin eq.)





**Validation** on **MUST campaign** (Mock Urban Setting Test), Utah's desert, USA. Presence of obstacles.

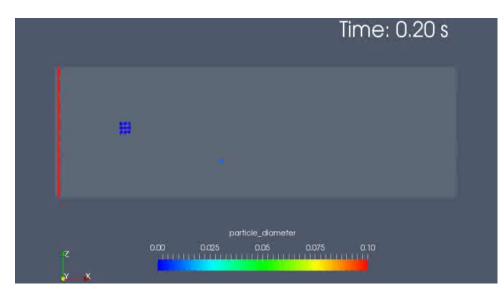


*Preliminary results for case 2681829 (neutral conditions)* Other tested cases: 2681849 (neutral conditions), 2640246 (stable conditions)

 $\square R_{ij}$ - $\varepsilon$  model with DFM (*Differential Flux Model*) for the scalars



# THANK YOU FOR YOUR ATTENTION



#### References:

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