



**COMPUTATIONAL FLUID DYNAMICS STUDY  
ON  
TWO-PHASE CO<sub>2</sub> DISPERSION  
IN A  
NEUTRAL ATMOSPHERE**

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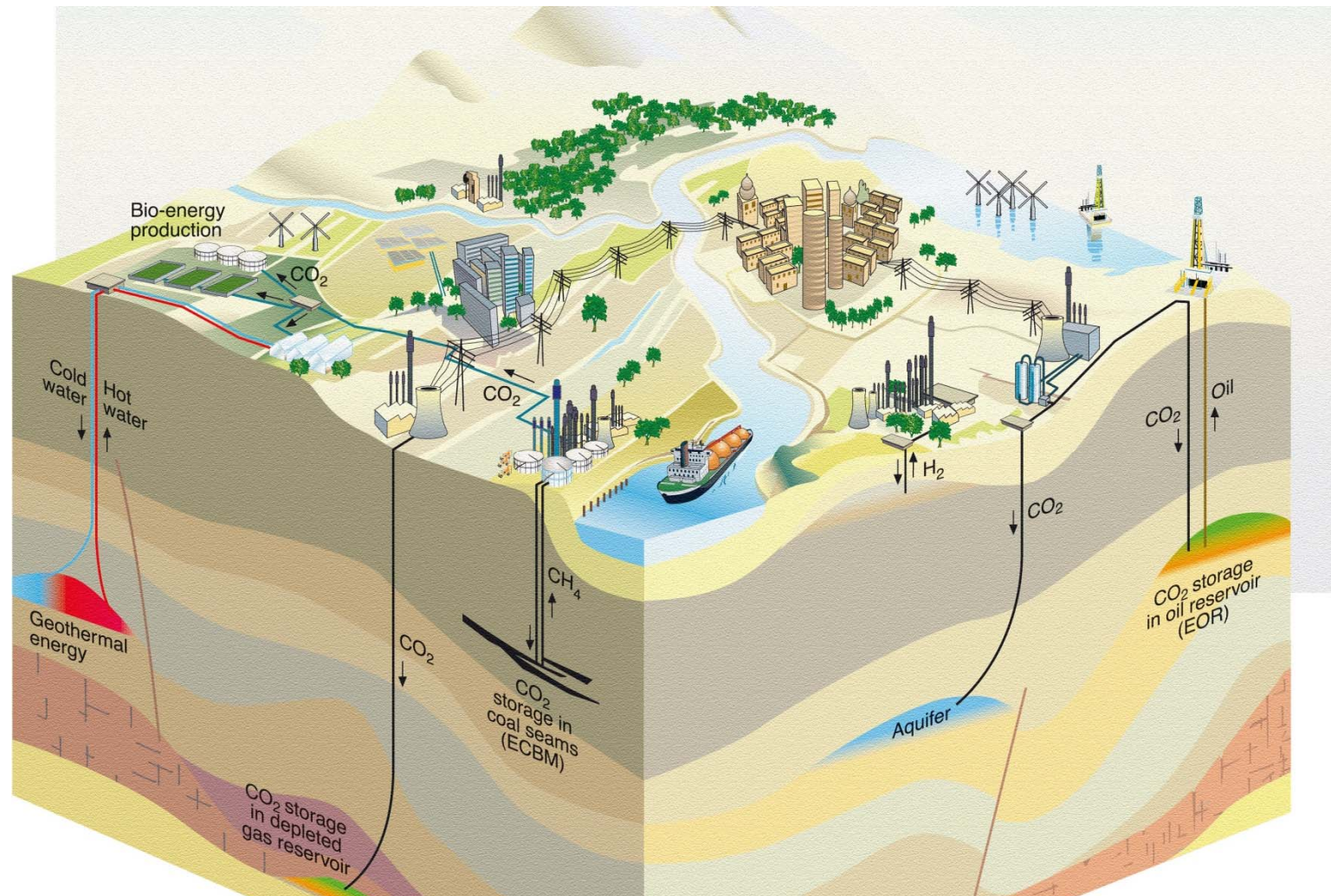


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- CFD in atmospheric conditions
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- Results:
  - ABL
  - Parameter study for release
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# CCS – Carbon Capture and Storage





## Toxicity properties of CO<sub>2</sub>

<b>Exposure time (min)</b>	<b>1% lethality (vol% CO<sub>2</sub>)</b>	<b>50% lethality (vol% CO<sub>2</sub>)</b>
1	11	15
10	8	11
30	7	9
60	6	8

Source: S. Connolly and L. Cusco, Hazards from high pressure carbon dioxide release during carbon dioxide sequestration processes, Proc. Int. Symp. Loss Prevention and Safety Promotion in the Process Industry, Edinburgh, 22-24 May 2007

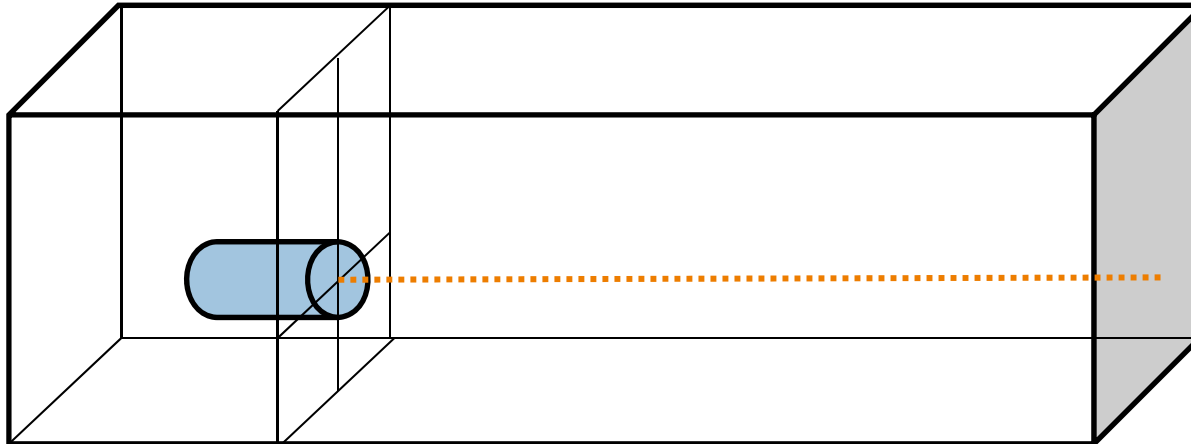


## CFD in atmospheric conditions

- Pre-requisite: correctly describe Atmospheric Boundary Layer (ABL) behaviour over domain:
  - Velocity
  - Turbulence
  - Temperature & pressure (non-neutral ABL)
- Recommendations from COST 732 (neutral ABL, RANS)
  - Computational grid
  - Domain extent and blockage
  - Boundary conditions



## Case Description



Test-case:

small scale release

Comparison-case:

large scale release



### Test case

Domain size: 300x100x50 m<sup>3</sup>  
Source location: 1 m height  
  
Initial pressure: 100 bar  
Initial temperature: 15 °C  
Source mass flow rate: 33 kg/s  
Source diameter: 5 cm  
Source temperature: 293 – 195 K  
Source solid fraction: 0 – 50 mass%



Fluent v12.1

2-phase model:  
Discrete Phase Model

Turbulence model: standard  $k\epsilon$

Cell sizes: 3 cm<sup>3</sup> - 120 m<sup>3</sup>  
Number of cells: 135 000

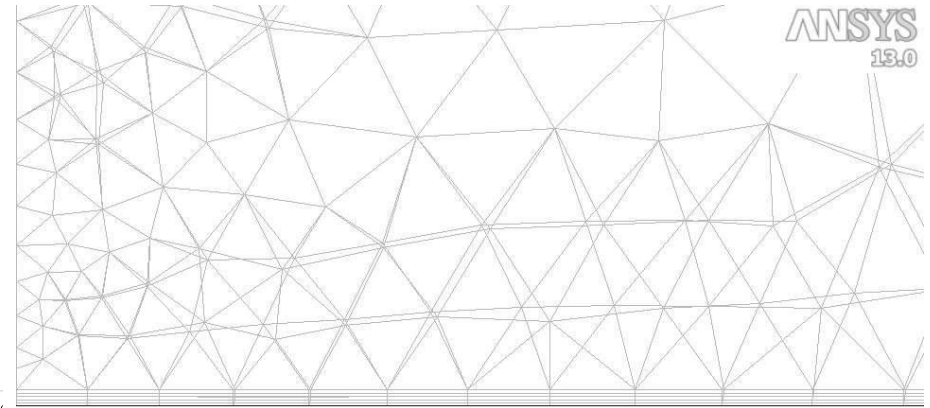
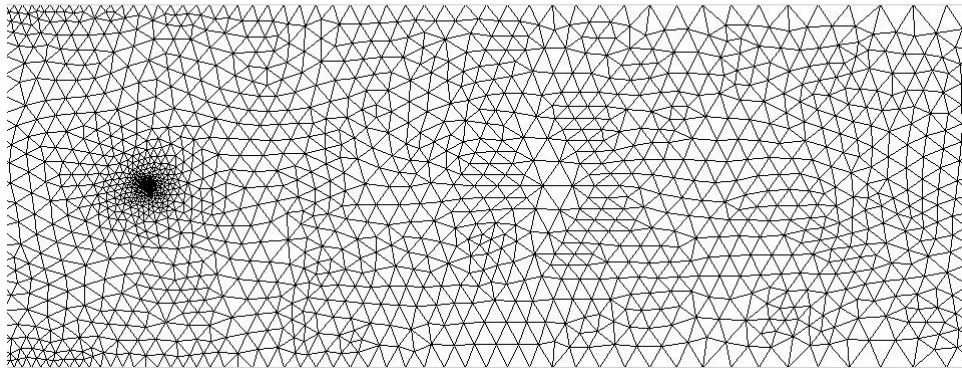
### Boundary conditions:

- Sides: symmetry planes
- Top: wall
- Inflow: velocity inlet
- Outflow: pressure outlet
- Bottom: wall with wall functions

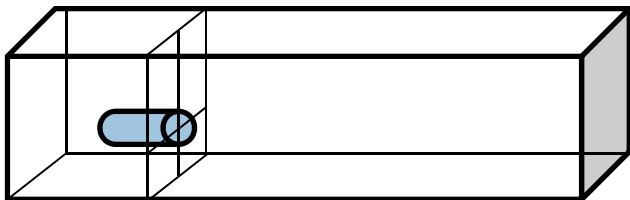
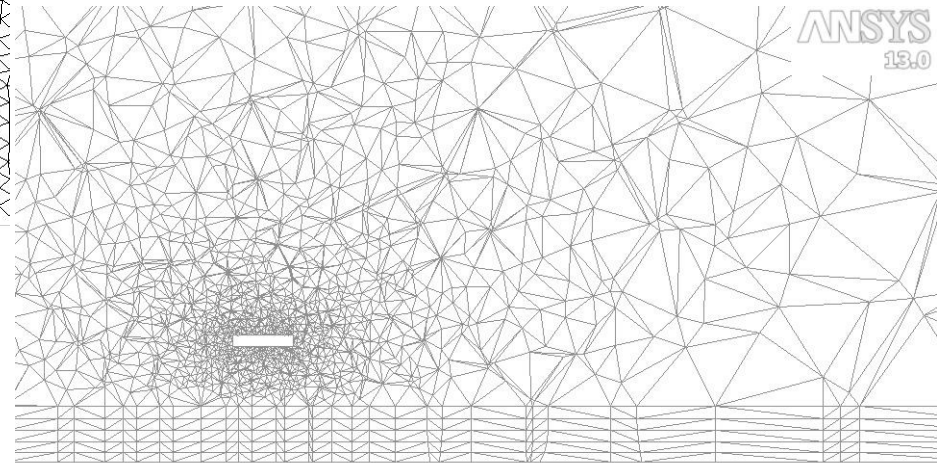


### Mesh

Bottom mesh



Mesh – side view







## Variations in test case

Several fraction of solid are used:

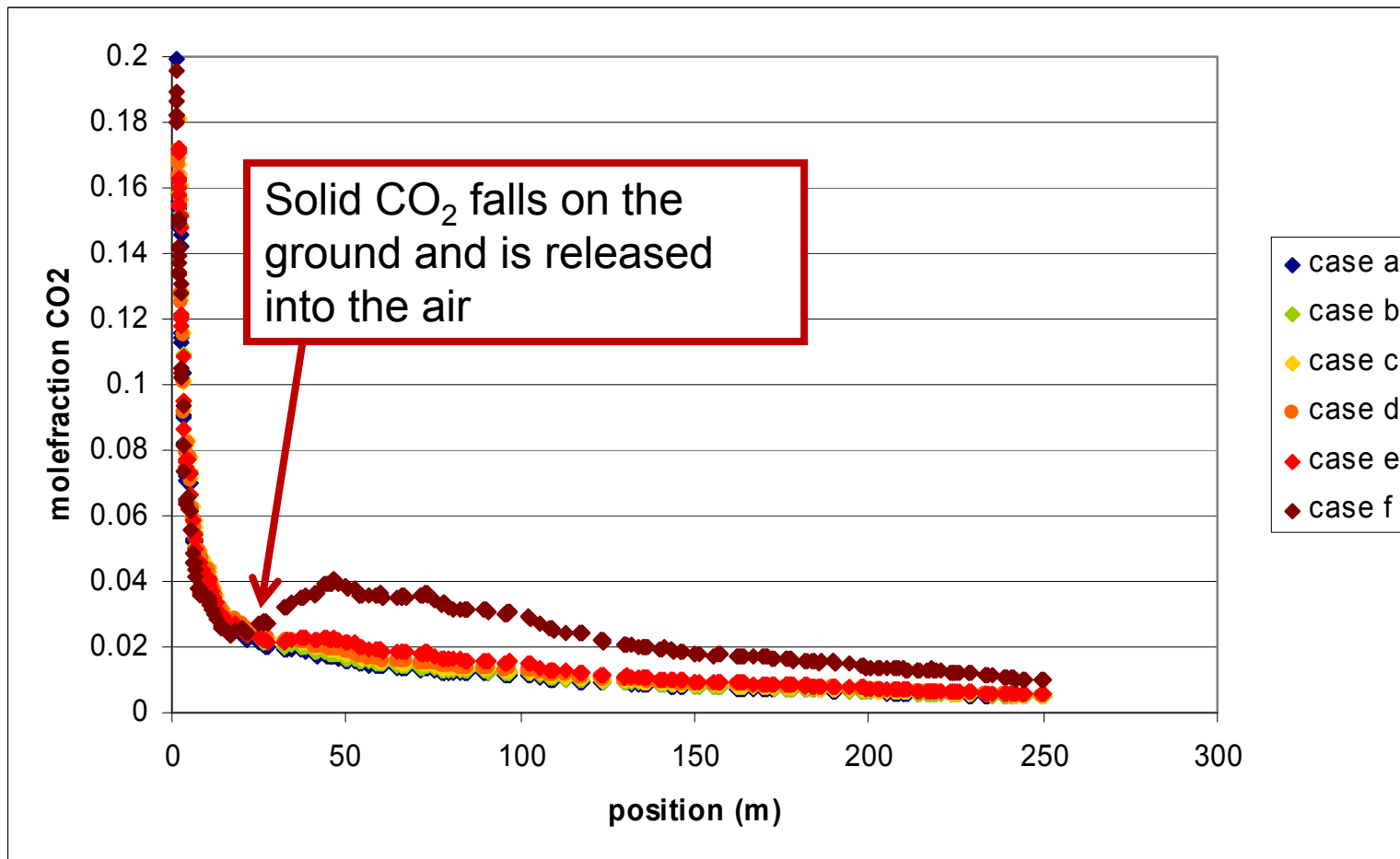
	Type of release	T (K)	%mass of solid
A	Gas	293	-
B	Gas	250	-
C	Gas	195	-
D	Gas + solid	195	1
E	Gas + solid	195	10
F	Gas + solid	195	50

With case F sensitivity studies are performed on the presence of solid particles:

- wall boundary conditions
- particle size
- gravity

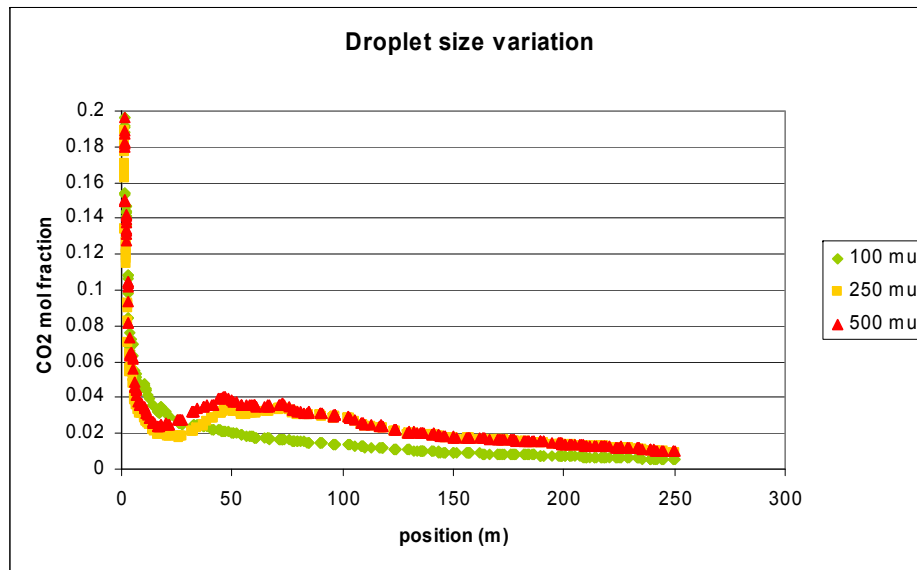


## CO<sub>2</sub> mole fraction for cases a-f



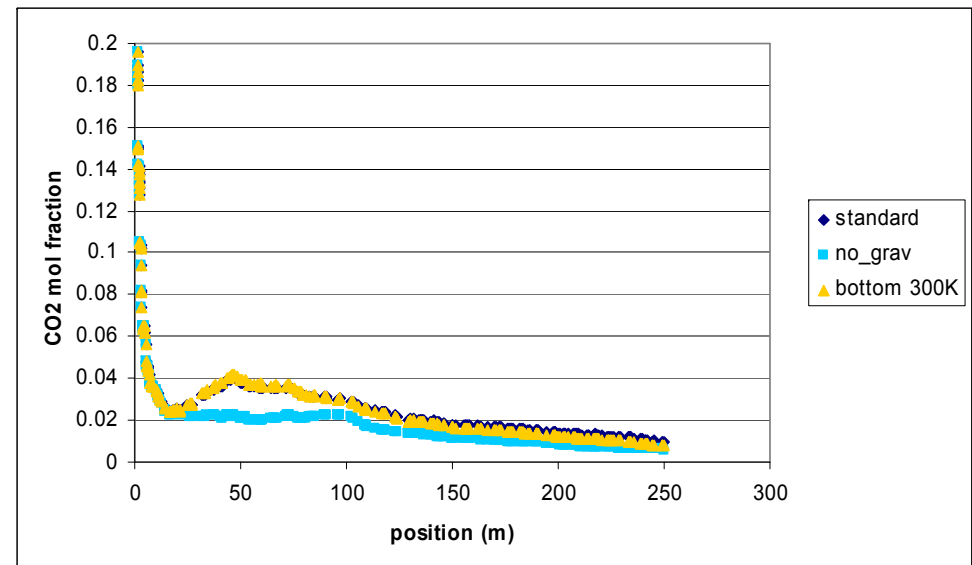


## Variations for sensitivity analysis



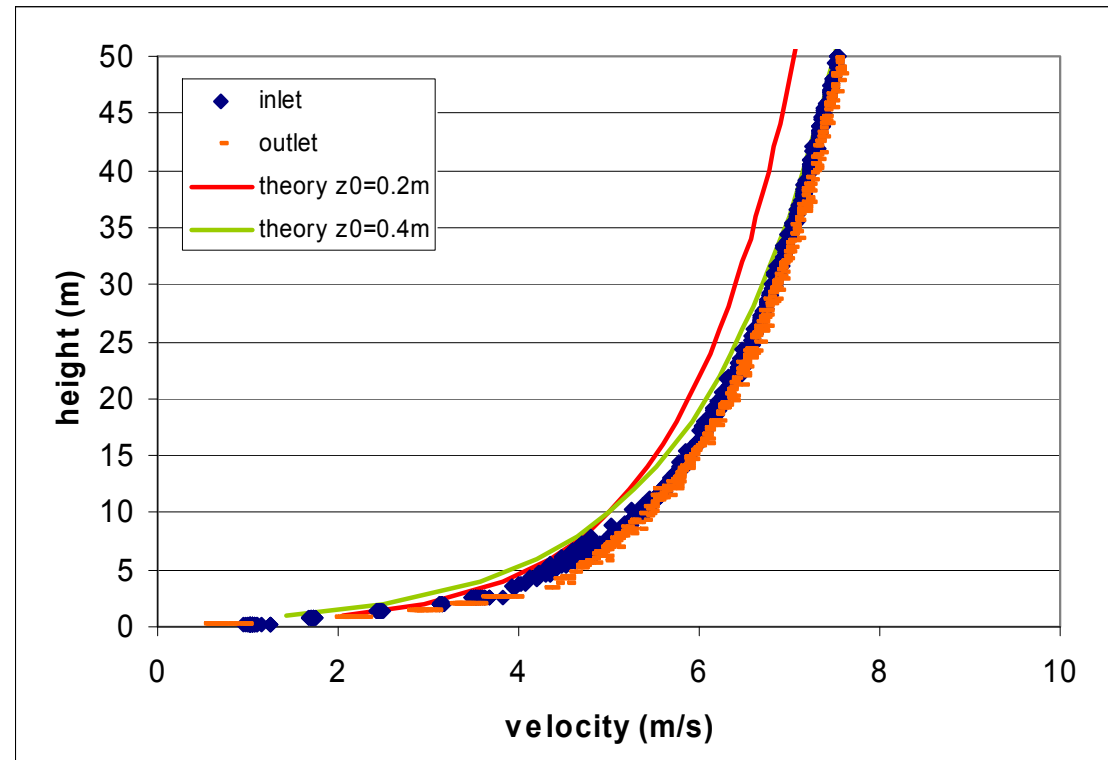
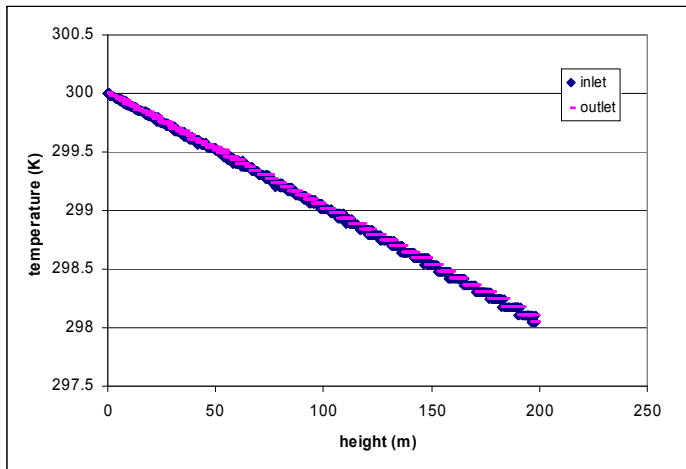
100  $\mu$  droplets do not rain out

Without gravity no rain out





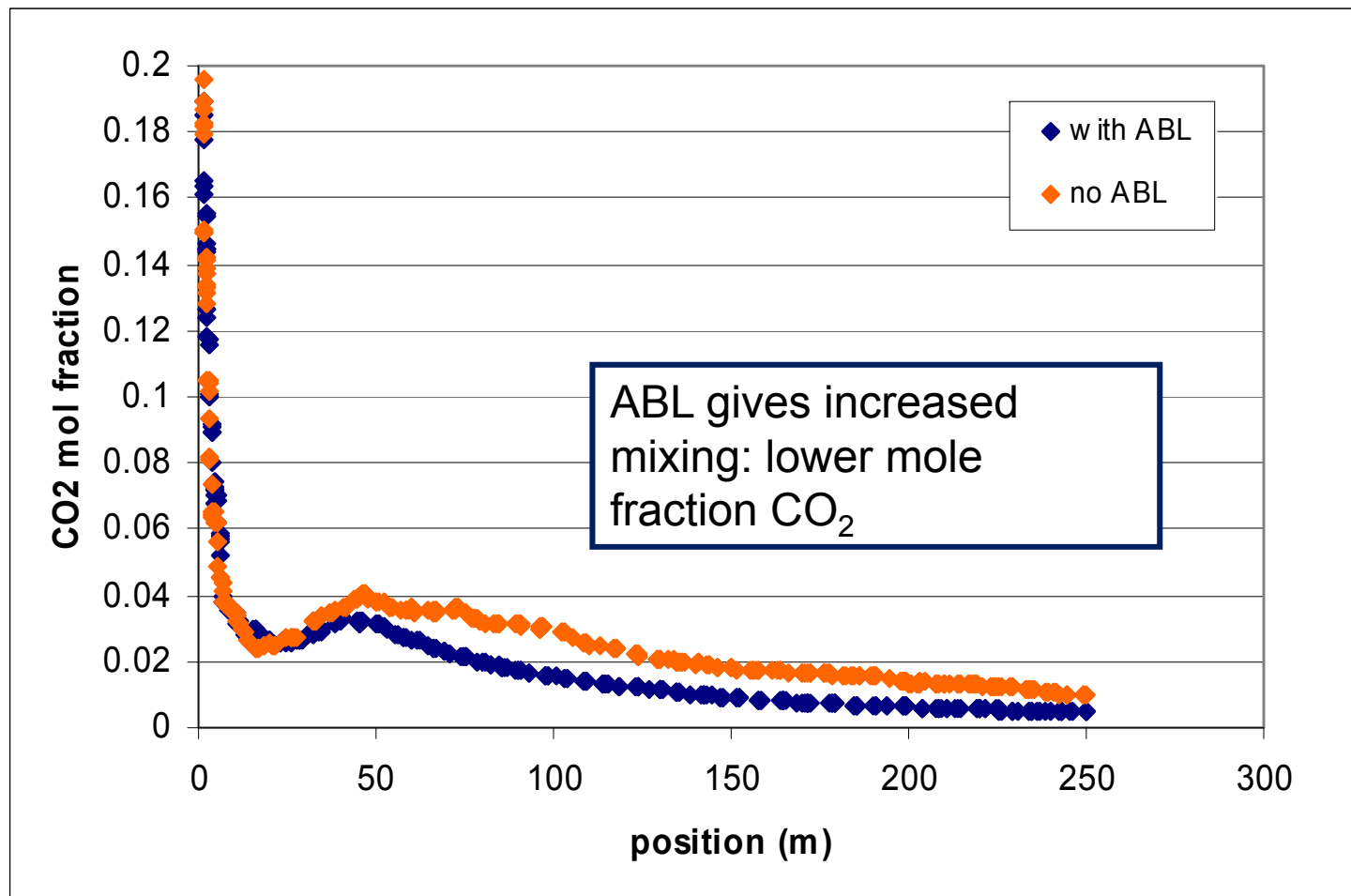
## Atmospheric Boundary layer: D5



- 2D ABL periodic conditions
- 3D ABL: 2D result at inlet
- Inlet = outlet velocity and temperature profile in 3D
- 2D profile 10% off from theoretical profile, increase mass flow will resolve this

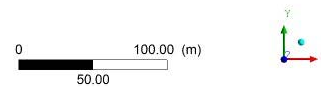
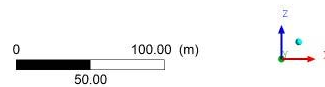
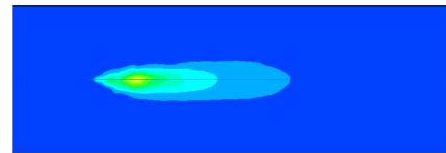
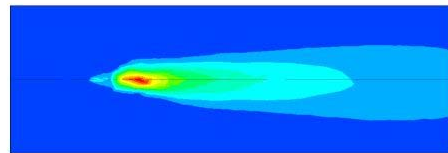
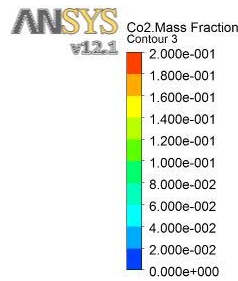
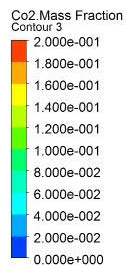


## Effect of ABL-modelling on concentration





## Top view of CO<sub>2</sub> mass fraction contours

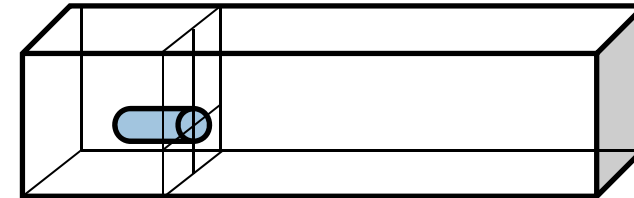


Uniform inlet velocity

D5 ABL



### Comparison case



Domain size: 800 x 400 x 200 m<sup>3</sup>  
Source location: 5 m height

Initial pressure: 150 bar  
Initial temperature: 20 °C  
Source mass flow rate: 5628 kg/s  
Source diameter: 298 cm  
Source temperature: 195 K  
Source solid fraction: 0 and 64.4 mass%

Fluent v12.1

2-phase model:  
Discrete Phase Model

Turbulence model: standard  $k\epsilon$

Cell sizes:  $3 \cdot 10^{-3} - 5 \cdot 10^3 \text{ m}^3$   
Number of cells: 175 000

### Boundary conditions:

- Sides: symmetry planes
- Top: velocity inlet
- Inflow: velocity inlet
- Outflow: pressure outlet
- Bottom: wall with wall functions

Source: T.A. Hill, J.E. Fackrell, M.R. Dubal, S.M. Stiff, Understanding the consequences of CO<sub>2</sub> leakage downstream of the powerplant, Energy Procedia (2010)



## Resulting volume%

	<b>Fluent vapour</b>	<b>Fluent 150 <math>\mu\text{m}</math></b>
200 m	8.9 %	10.4 %
300 m	6.6 %	7.1 %
400 m	5.2 %	5.3 %

- Including particles increases effect distances





## Resulting volume%

	<b>Fluent vapour</b>	<b>Fluent 150 <math>\mu\text{m}</math></b>	<b>CFX vapour</b>	<b>CFX 50 -150 <math>\mu\text{m}</math></b>
200 m	8.9 %	10.4 %	15.5 %	18.6 %
300 m	6.6 %	7.1 %	11.0 %	12.1 %
400 m	5.2 %	5.3 %	8.2 %	8.1 %

- Including particles increases effect distances (Fluent and CFX)
- No experimental data available for validation



## Resulting volume%

	<b>Fluent vapour</b>	<b>Fluent 150 µm</b>	<b>CFX vapour</b>	<b>CFX 50 -150 µm</b>	<b>Phast</b>
200 m	8.9 %	10.4 %	15.5 %	18.6 %	11.3 %
300 m	6.6 %	7.1 %	11.0 %	12.1 %	8.1 %
400 m	5.2 %	5.3 %	8.2 %	8.1 %	6.4 %

- Including particles increases effect distances (Fluent and CFX)
- No experimental data available for validation
- CFX over estimates with respect to Phast, Fluent underestimates with respect to Phast

Source Phast and CFX data: T.A. Hill, J.E. Fackrell, M.R. Dubal, S.M. Stiff,  
Understanding the consequences of CO<sub>2</sub> leakage downstream of the  
powerplant, Energy Procedia (2010)



## Differences in CFD calculations

- Particle size (single value or distribution)
- Description ABL
- Level of turbulence in jet



## Conclusions

- Method is shown to perform CFD on dispersion of evaporating particles in atmospheric conditions
- Only verification with integral model and other CFD model is done: good comparison
- Continue development of CFD for atmospheric dispersion