

**ATMOSPHERIC DISPERSION AND  
INDIVIDUAL EXPOSURE OF  
HAZARDOUS MATERIALS.  
*VALIDATION AND INTERCOMPARISON STUDIES***

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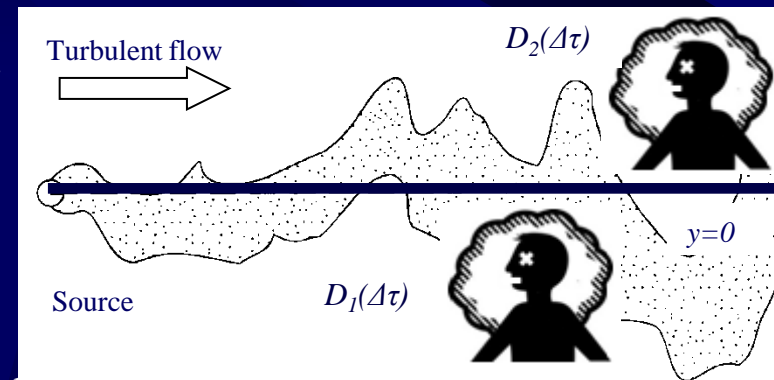
# Motivation

- Deliberate or accidental atmospheric release from a near ground point source upwind or in a complex urban environment.



- Prediction of individual exposure at a time interval  $\Delta\tau$  downwind the source (Sensor 1, 2).
- Individual exposure = Dosage at a time interval  $\Delta\tau$ .

$$D(\Delta\tau) = \int_0^{\Delta\tau} C(t) dt$$



# The problem

Stochastic nature of turbulence



Concentration variability

Conclusion:

The prediction of actual concentration/dosage downwind the source is practically impossible.

EWTL, University of Hamburg

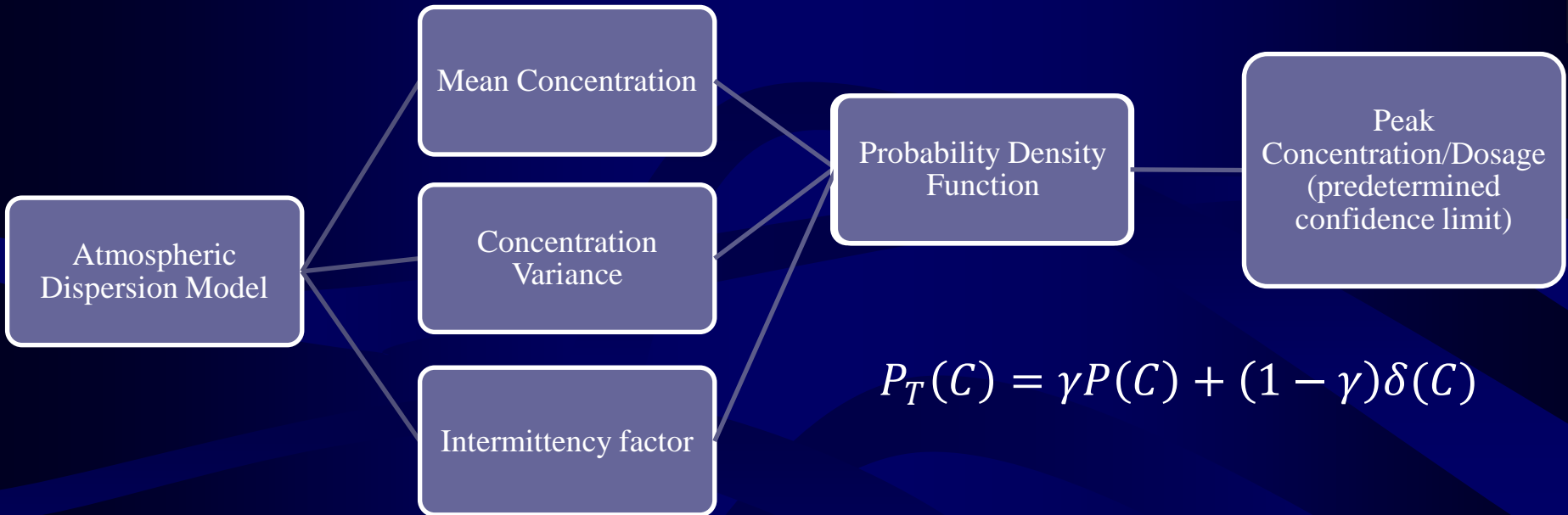
Maximum individual exposure/expected dosage:

$$D_{\max}(\Delta\tau) = \left[ \int_0^{\Delta\tau} C(t) dt \right]_{\max} = C_{\max}(\Delta\tau) \Delta\tau$$

$C_{\max}(\Delta\tau)$  is the peak time averaged concentration.

# Predicting maximum dosage

## The Probabilistic Models



$$P_T(C) = \gamma P(C) + (1 - \gamma)\delta(C)$$

Research	Gamma	Lognormal	Weibull	Exponential	Chopped normal
Lung et al., (1992)	x	x	x		
Mylne & Mason (1991)				x	x
Yee (1990)		x		x	x
Yee et al., (1993)	x	x	x	x	x
Gailis et al., (2007)	x	x			
Gailis & Hill (2006)	x			x	x

Gamma:  $P_T(C|a,b) = \frac{1}{b^a \Gamma(a)} C^{a-1} e^{-C/b}$

Lognormal:  $P_A(C) = \frac{1}{C \sqrt{C^2} \sqrt{2\pi}} e^{-\frac{(\ln C - \bar{c})^2}{2C^2}}$

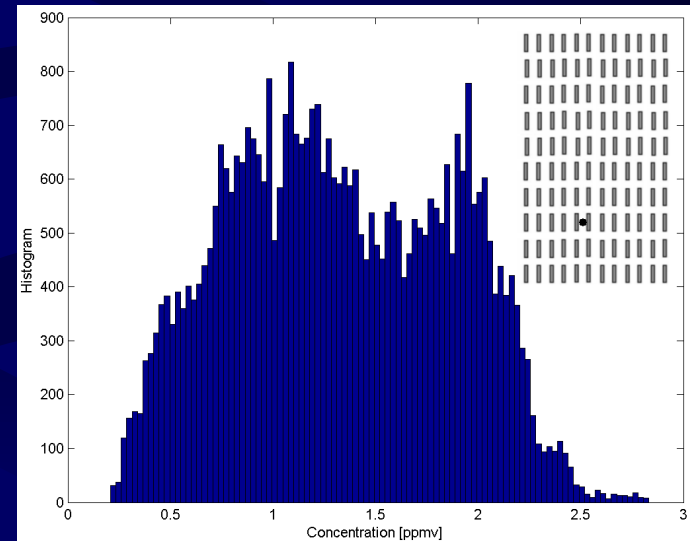
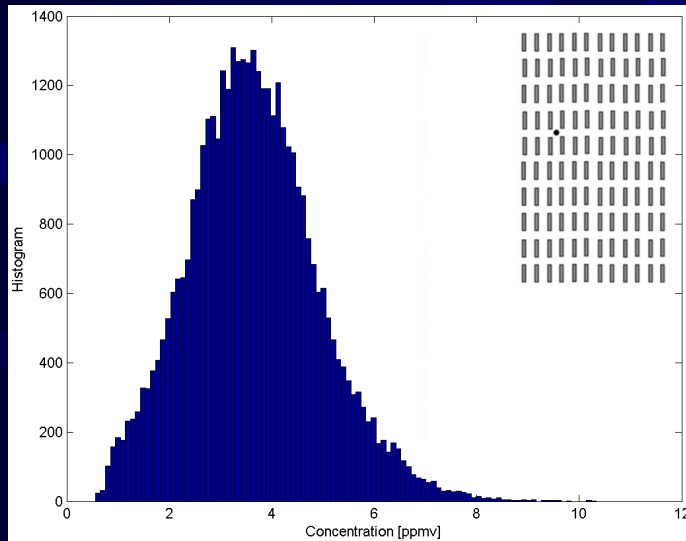
Weibull:  $P_W(C) = ba^{-b} C^{b-1} e^{-\left(\frac{C}{a}\right)^b}$

Exponential:  $P_E(C) = \frac{1}{C} e^{-\frac{C}{c}}$

Chopped normal:  $P_A(C) = \frac{4}{\sqrt{2\pi} \sqrt{C^{12}}} e^{-\frac{(c-\bar{c})^2}{2C^2}}$

# Limits of probabilistic method

- There is not a common well known distribution that can be used to describe the concentration in all the locations.



2. Results sensitive to the confidence interval 95%, 99%, 99.8%, 99.98%.

For 100%  $C_{max} \rightarrow \infty$

# Predicting maximum dosage

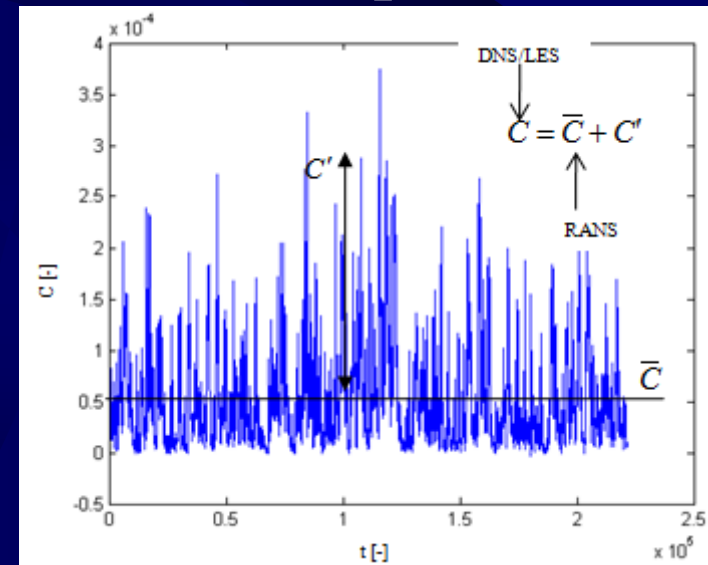
## The Deterministic Models (Bartzis et al., 2008)

$$\frac{D_{\max}(\Delta\tau)}{\bar{C}} = f\left(I, \frac{\Delta\tau}{T_c}\right) \longrightarrow D_{\max}(\Delta\tau) = \bar{C} \left[ 1 + \beta I \left(\frac{\Delta\tau}{T_c}\right)^{-n} \right] \Delta\tau$$

- Turbulence autocorrelation time scale  $T_c = \int_0^{\infty} R_c(\tau) d\tau$
- Autocorrelation function  $R_c(\tau) = \frac{C'(t)C'(t+\tau)}{\overline{C'^2}}$
- Mean value:  $\bar{C}$  Fluctuation:  $C'$  Variance:  $\overline{C'^2}$
- Fluctuation intensity:  $I = \overline{C'^2} / \bar{C}^2$
- $\beta$  and  $n$  are parameters that are estimated experimentally  
FLADIS:  $\beta = 1.5, n = 0.3$   
MUST:  $\beta = 1.64, n = 0.3$

# The prediction requirements

- The mean concentration  $\bar{c}$
- The concentration variance  $\overline{c'^2}$
- The turbulent time scales  $T_C$
  
- The simplest and practical approach for complex terrains
  - CFD RANS models
  - Two-equation turbulent closure



# Transport equation for concentration variance

*(using the concept of eddy viscosity/diffusivity)*

$$\underbrace{\frac{\partial \rho \overline{C'^2}}{\partial t}}_{\text{Change in time}} + \underbrace{\frac{\partial \rho \overline{u_i C'^2}}{\partial x_i}}_{\text{Advection by the mean velocity field}} = \underbrace{-2\rho K_c \left( \frac{\partial \overline{C}}{\partial x_i} \right)^2}_{\text{Generation of fluctuations due to gradients in the mean concentration}} + \frac{\partial}{\partial x_i} \left[ \underbrace{\rho (K_c + D)}_{\text{Diffusive transport produced by turbulent velocity fluctuations}} \frac{\partial \overline{C'^2}}{\partial x_i} \right] - \underbrace{2\rho D \frac{\partial \overline{C'}}{\partial x_i} \frac{\partial \overline{C'}}{\partial x_i}}_{\text{Dissipation by molecular diffusion of the fine scale concentration fluctuations}}$$

Turbulent concentration fluxes:

$$\underbrace{-\overline{u'_i C'^2}}_{\text{Diffusive transport produced by turbulent velocity fluctuations}} = K_c \frac{\partial \overline{C'^2}}{\partial x_i} = K_c \frac{\partial \overline{C'^2}}{\partial x_i} = \frac{K_m}{\sigma_h} \frac{\partial \overline{C'^2}}{\partial x_i}$$



# The dissipation rate of concentration variance

The usual approach → algebraic modelling (Csanady, 1967):

$$2D \frac{\overline{\partial C' \partial C'}}{\partial x_i \partial x_i} = \frac{\overline{C'^2}}{T_{dc}}$$

$T_{dc}$  = dissipation time scale of concentration variance

# The dissipation rate of concentration variance:

*A new approach (Efthimiou & Bartzis, 2011)*

$$\frac{T_{dc}}{T_{dc\infty}} = \frac{T_C}{T_{C\infty}}$$

*Assumptions:*

1. The time scales  $T_{dc}$  and  $T_C$  are analogous variables.
2. The time scales  $T_{dc}$  and  $T_C$  depends on the pollutant travel time.
3. The time scales  $T_{dc\infty}$  and  $T_{C\infty}$  correspond to full mixing conditions and depends on the flow turbulent characteristics.

The new approach has been tested until now with the  $k$ - $\zeta$  model (Bartzis, 2005).

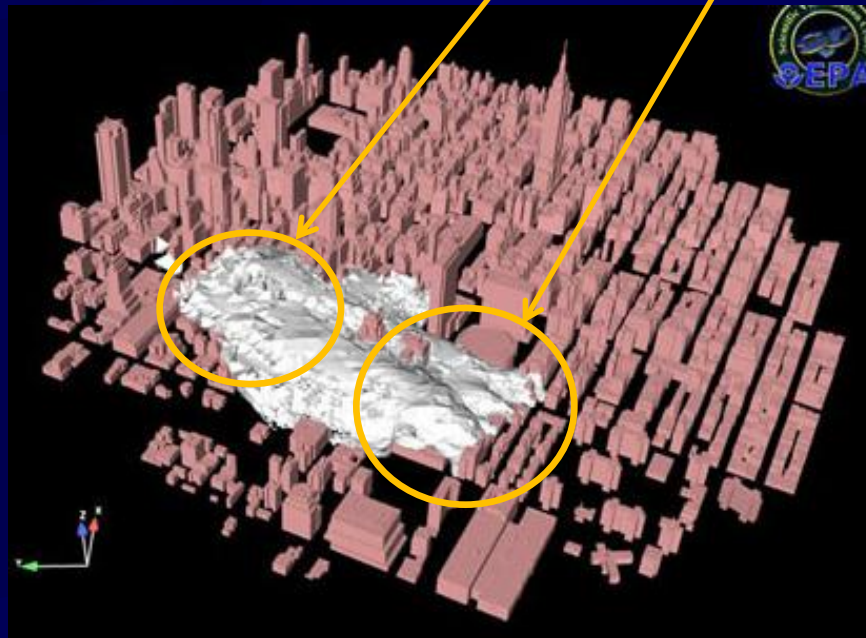
In the present study: Incorporation of the widely used  $k$ - $\varepsilon$  model (Launder, B. E. and D. B. Spalding, 1974) to the new methodology.

# The autocorrelation time scale $T_C$

Experimental evidence:  $T_C$  is highly correlated with the pollutant travel time especially near the source.

$$T_C = \min(c_u T_{travel}, T_{C\infty})$$

$$c_u = 0.11$$



# Pollutant travel time

## *Radioactive tracer method*

### Remarks:

1. In Eulerian CFD models the estimation of the pollutant travel time is not direct.
2. The use of the physical law  $x/U$  is questionable in complex urban environments.

### Radioactive tracer method

- Two tracers are released simultaneously from the same source with the same experimental conditions.
- One tracer is considered passive ( $C_0$ ) while the other is considered radioactive ( $C$ ) with a decay constant  $\lambda$  ( $s^{-1}$ ).

Pollutant travel time:

$$T_{travel} = -\frac{1}{\lambda} \ln \frac{C}{C_0}$$

# The time scale $T_{C\infty}$ (full mixing)

**$k$ - $\zeta$  model** (Efthimiou et al., 2011)

$$T_{C\infty} = c_h k^{-1/2} \zeta^{-1} \quad c_h = 1.0$$

**Standard  $k$ - $\varepsilon$  model** (Andronopoulos et al., 2002, Milliez and Carissimo, 2008)

$$T_{C\infty} = k \varepsilon^{-1}$$

# The time scale $T_{dc\infty}$ (full mixing)

$$T_{dc\infty} = c_{dc} T_{C\infty}$$

**$k$ - $\zeta$  model:**

Efthimiou et al., 2011:  $c_{dc} = 3.05$

**Standard  $k$ - $\varepsilon$  model:**

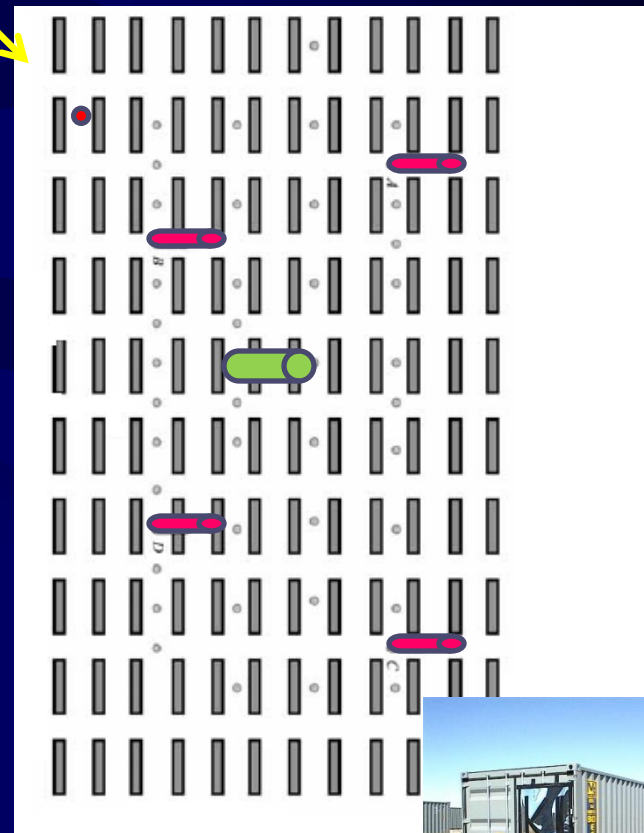
Andronopoulos et al., 2002:  $c_{dc} = 0.8$

Milliez and Carissimo, 2008:  $c_{dc} = 1.0$

# The MUST experiment (Yee & Bilstoft, 2004)

- 40 locations on 4 horizontal sampling lines (at  $z = 1.6$  m)
- 8 sensors on 32-m central tower (at  $z = 1, 2, 4, 6, 8, 10, 12, 16$  m)
- 6 sensors on each of 6-m tower at A, B, C, D (at  $z = 1, 2, 3, 4, 5, 5.9$  m)

Approach flow



# The selected validation trials

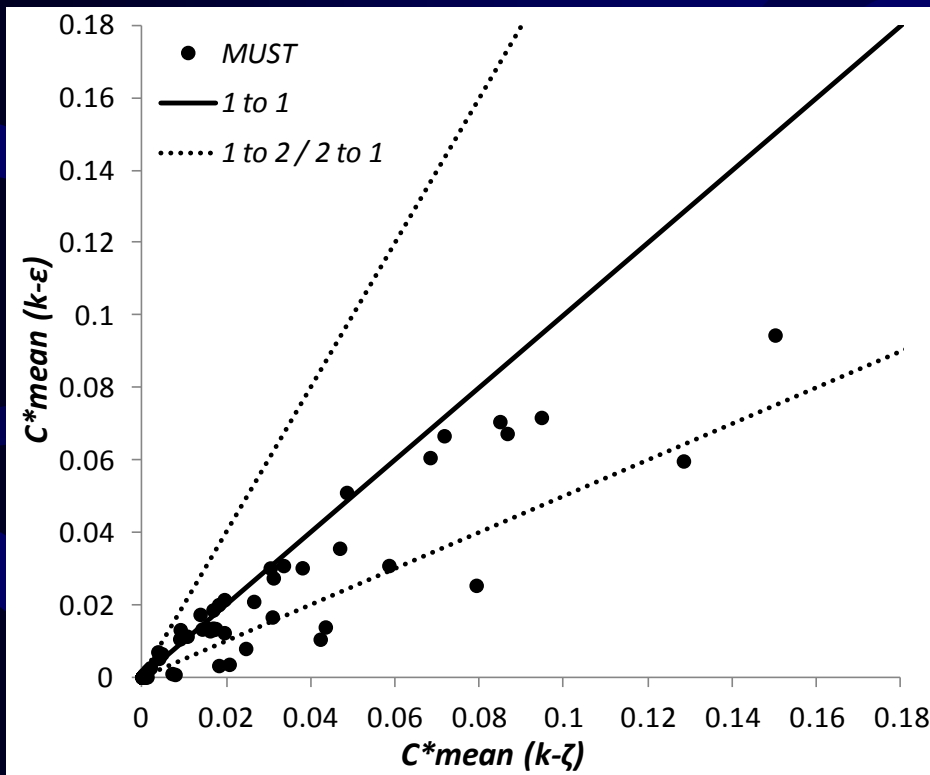
Experimental parameters	MUST	
	Trial 11	Trial 12
Date	25/9/2001	25/9/2001
Hour of emission	18:29:00	18:49:00
Tracer	Propylene (C <sub>3</sub> H <sub>6</sub> )	
Emission duration	15 min	
Emission rate	0.00457 kg s <sup>-1</sup>	
Source area	0.00196 m <sup>2</sup>	
Source height	1.8 m	0.15 m
Reference velocity	7.93 m s <sup>-1</sup>	7.26 m s <sup>-1</sup>
Wind direction	-40.54°	-41.23°
Mean atmospheric temperature	304.94 K	304.32 K
Roughness height	0.127 m	0.086 m
Manipulation time period	200 s	
Friction velocity	0.92 m s <sup>-1</sup>	0.76 m s <sup>-1</sup>
Monin-Obukhov length	-28000 m	2500 m
Exponential exponent	0.25	0.23

The simulations are performed with the CFD code ADREA (Bartzis et al., 1991).

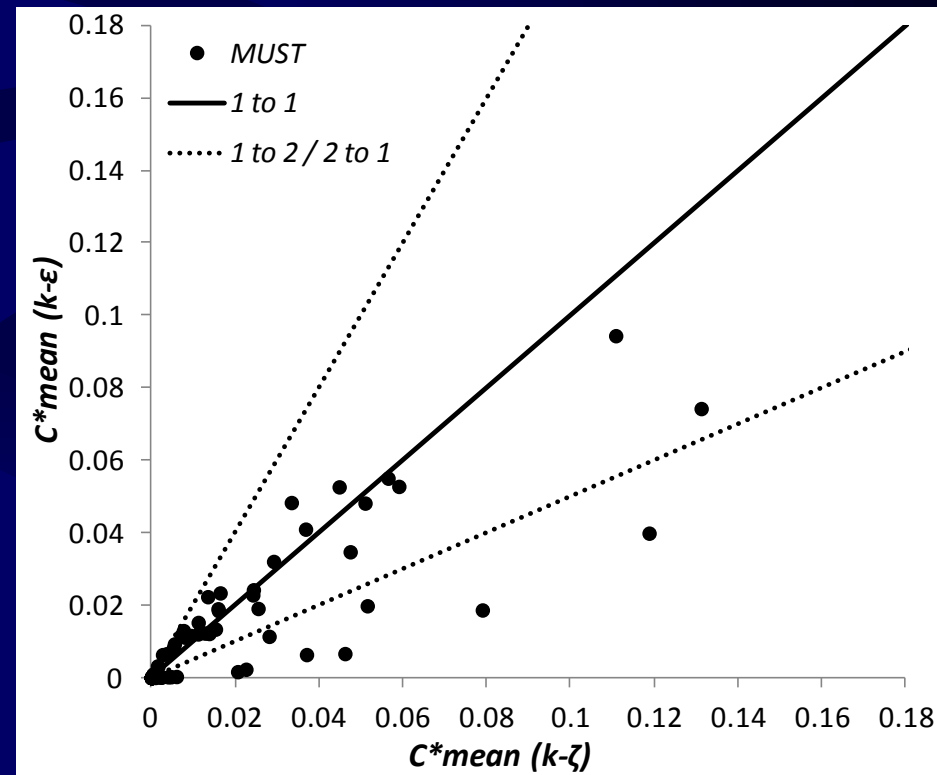


# Mean concentration results (I)

## Trial 11



## Trial 12



# Mean concentration results (II)

Factor of two of observations

$$FAC2 = \frac{N}{n} = \frac{1}{n} \sum_{i=1}^n N_i$$

$$N_i \begin{cases} 1, & 0.5 \leq \frac{C_{pi}}{C_{oi}} \leq 2.0 \\ 0, & \frac{C_{pi}}{C_{oi}} < 0.5 \text{ } \dot{\vee} \text{ } \frac{C_{pi}}{C_{oi}} > 2.0 \end{cases}$$

Fractional Bias

$$FB = \frac{(\overline{C_o} - \overline{C_p})}{0.5(\overline{C_o} + \overline{C_p})}$$

Quality acceptance criteria (Schatzmann et al., 2010)  $|FB| < 0.3$   
 $NMSE < 4$   
 $FAC2 > 0.5$

(underestimation/overestimation)

Normalized mean square error (dispersion)

$$NMSE = \frac{(\overline{C_o - C_p})^2}{\overline{C_o C_p}}$$

	Validation metrics		
	FAC2	FB	NMSE
<b>Near ground measurements</b>			
Trial 11 ( $k-\zeta / k-\varepsilon$ )	0.60 / 0.43	-0.08 / 0.52	0.35 / 0.77
Trial 12 ( $k-\zeta / k-\varepsilon$ )	0.89 / 0.52	-0.22 / 0.39	0.33 / 0.53
<b>Total measurements</b>			
Trial 11 ( $k-\zeta / k-\varepsilon$ )	0.48 / 0.44	-0.24 / 0.11	0.69 / 0.73
Trial 12 ( $k-\zeta / k-\varepsilon$ )	0.70 / 0.46	-0.19 / 0.12	0.42 / 0.53

# Concentration standard deviation results (I)

$$T_{dc\infty} = c_{dc} T_{C\infty}$$

Selection of the parameter  $c_{dc}$ :

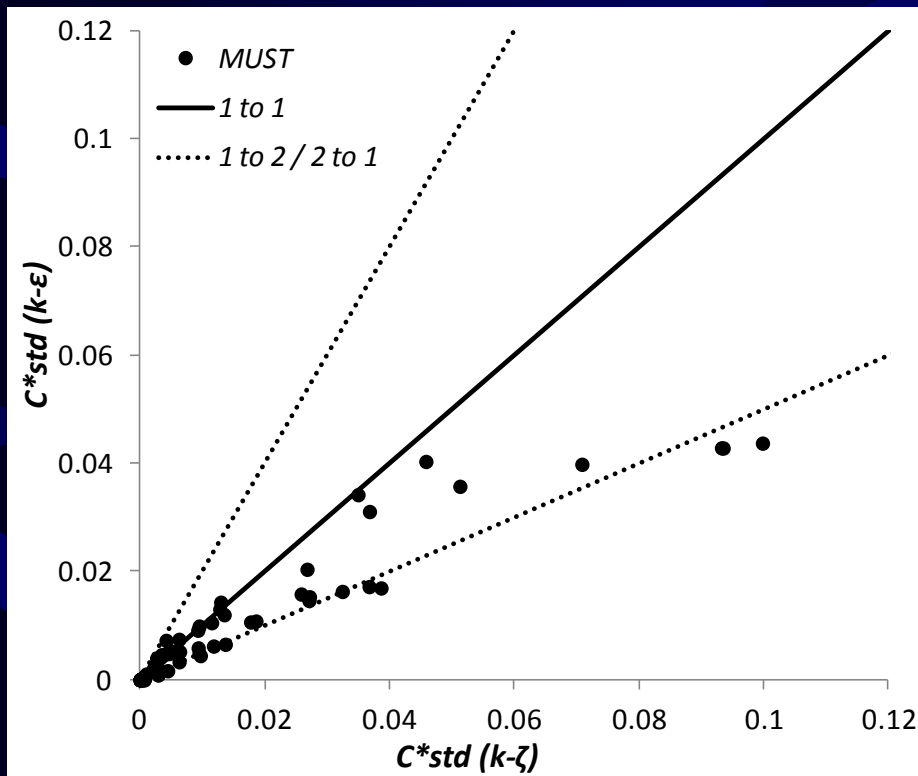
Sensitivity study on the influence of this parameter to the results has been performed for both Trials using the  $k$ - $\varepsilon$  model.

**First simulation:**  $c_{dc} = 0.8 \rightarrow$  underprediction (e.g. for Trial 11 and for all sensors: FAC2 = 5.7%, NMSE = 2.49, FB = 1.03).

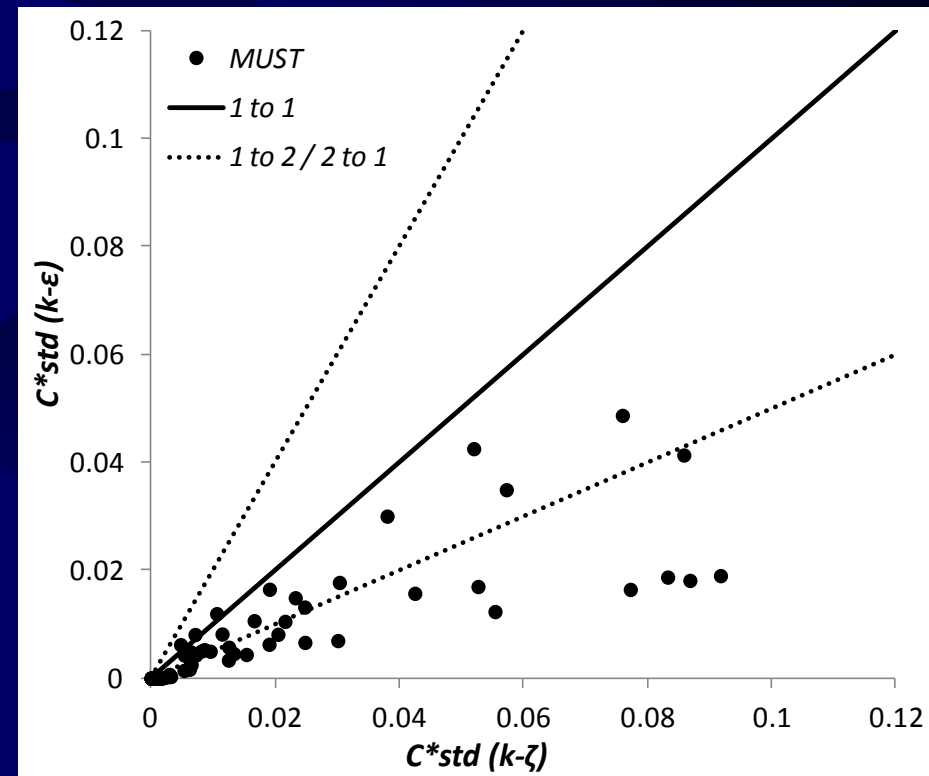
**Best performance:**  $c_{dc} = 1.7$ .

# Concentration standard deviation results (II)

## Trial 11



## Trial 12



# Concentration standard deviation

## results (III)

Factor of two of observations

$$FAC2 = \frac{N}{n} = \frac{1}{n} \sum_{i=1}^n N_i$$

$$N_i \begin{cases} 1, & 0.5 \leq \frac{C_{pi}}{C_{oi}} \leq 2.0 \\ 0, & \frac{C_{pi}}{C_{oi}} < 0.5 \text{ } \dot{\vee} \text{ } \frac{C_{pi}}{C_{oi}} > 2.0 \end{cases}$$

Fractional Bias

$$FB = \frac{(\overline{C_o} - \overline{C_p})}{0.5(\overline{C_o} + \overline{C_p})}$$

Quality acceptance criteria (Schatzmann et al., 2010)  $|FB| < 0.3$   
 $NMSE < 4$   
 $FAC2 > 0.5$

(underestimation/overestimation)

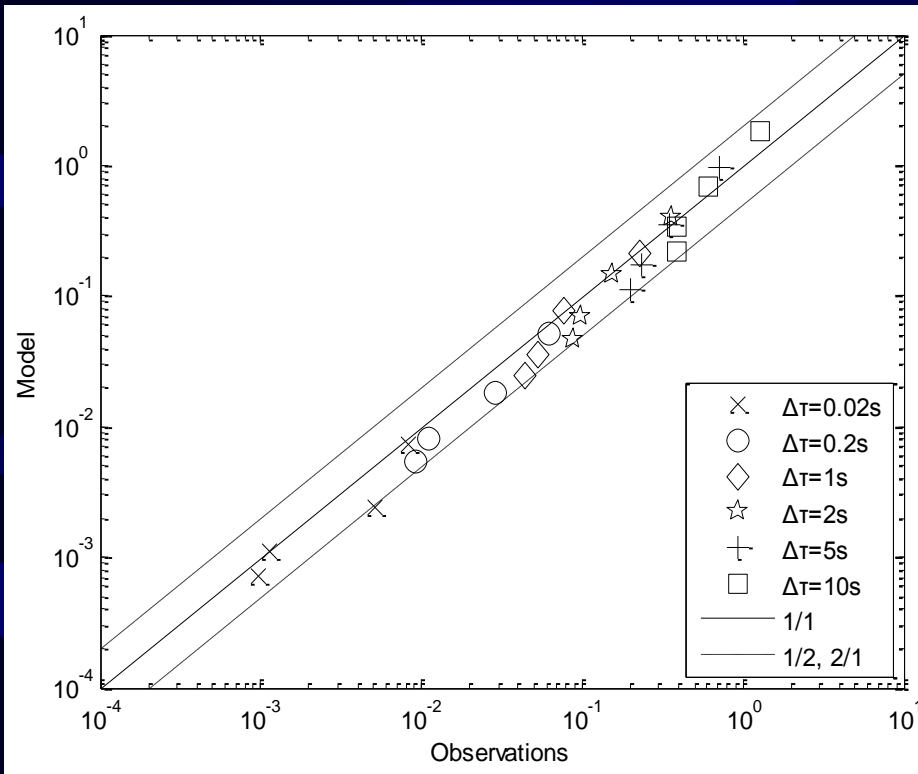
Normalized mean square error (dispersion)

$$NMSE = \frac{(\overline{C_o - C_p})^2}{\overline{C_o C_p}}$$

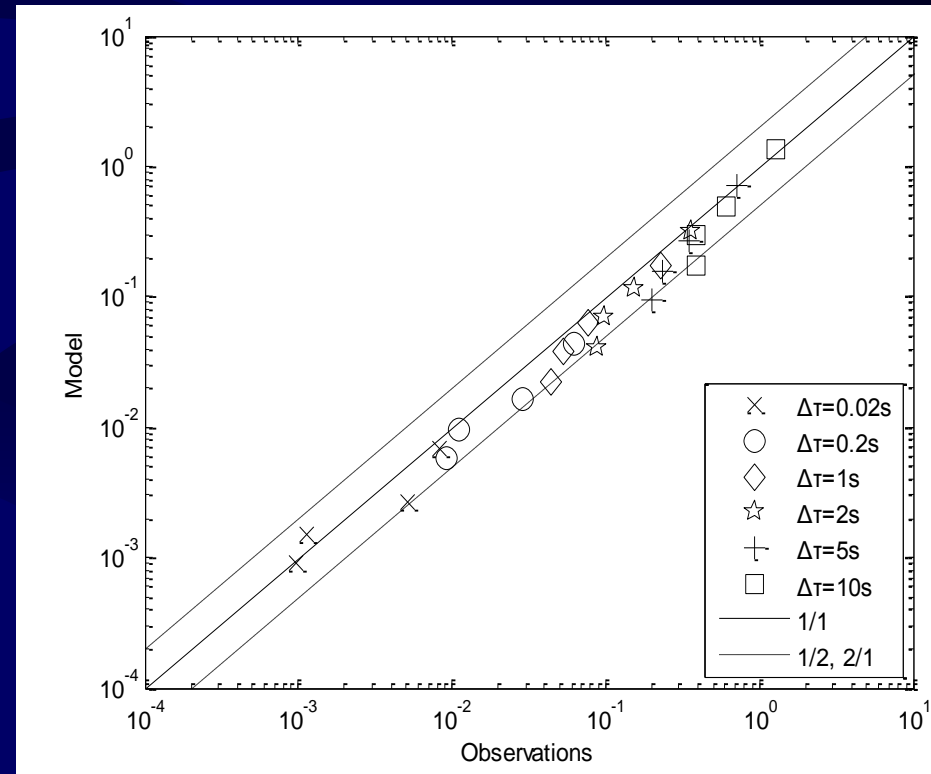
	Validation metrics		
	FAC2	FB	NMSE
<b>Near ground measurements</b>			
Trial 11 ( $k-\zeta / k-\varepsilon$ )	0.63 / 0.60	0.21 / 0.37	0.22 / 0.35
Trial 12 ( $k-\zeta / k-\varepsilon$ )	0.82 / 0.67	0.075 / 0.19	0.088 / 0.17
<b>Total measurements</b>			
Trial 11 ( $k-\zeta / k-\varepsilon$ )	0.59 / 0.69	-0.33 / 0.12	1.39 / 0.26
Trial 12 ( $k-\zeta / k-\varepsilon$ )	0.76 / 0.68	-0.35 / -0.047	1.20 / 0.34

# Individual exposure

## Trial 11



## Trial 12



# Conclusions

- The proposed approach on concentration time scale dependency on pollutant travel time seems to be a valid approximation in predicting plume dispersion from a point source in CFD RANS modeling using the  $k$ - $\zeta$  and standard  $k$ - $\varepsilon$  turbulence models.
- In case of  $k$ - $\varepsilon$  model a new value for  $c_{dc}$  1.7 allowed a good insight into the fluctuation results.
- The validation study was performed against MUST field experimental data under neutral conditions.
- An overall better performance for concentration mean and standard deviation was observed when the  $k$ - $\zeta$  model was used.
- More validation and intercomparison studies are planned by the authors.