

# A Lagrangian stochastic model for estimating the high order statistics of a fluctuating plume in the neutral boundary layer

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- 3 Numerical modelling
- 4 Numerical experiments
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- Impact assessment of risks related to the dispersion of flammable gases and toxic substances.
- Simulation of the combined effects of the turbulent mixing and molecular diffusivity.
- Estimate of the concentration fluctuations and prediction of the higher statistics and the concentration PDFs.

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# References

- M. Cassiani, P. Franzese, U. Giostra, 2005a. A PDF micromixing model of dispersion for atmospheric flow. Part I: development of model, application to homogeneous turbulence and to a neutral boundary layer. *Atmos. Environ.* **39**, 1457-1469.
- J.V. Postma, J.D. Wilson, E. Yee, 2011a. Comparing two implementations of a micromixing model. Part I: wall shear-layer flow. *Bound.-Layer Meteor.* **140**, 207-224.
- J.E. Fackrell, A. Robins, 1982. Concentration fluctuations and fluxes in plumes from point sources in a turbulent boundary later. *J. Fluid Mech.* **117**, 1-26.
- B.L. Sawford, 2004. Micro-mixing modeling of scalar fluctuations for plumes in homogeneous turbulence. *Flow Turbul. Combust.* **72**, 133-160.

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# Current study

New experiment data set in wind tunnel:

- Measures of high order concentration statistics in a fluctuating plume in a neutral boundary layer.
- Poster session T8.

Numerical simulations:

- Comparison between experiments and computed solutions.
- Evaluation of the accuracy of the model.

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# Lagrangian Stochastic model

Equations describing the evolution of the position  $X_i$  and velocity  $U_i$  of a set of independent fluid particles.

$$dX_i = (\langle u_i \rangle + U'_i) dt$$

deterministic term      stochastic diffusive term

$$dU'_i = \overbrace{a_i(\mathbf{X}, \mathbf{U}', t) dt} + \overbrace{b_{ij}(\mathbf{X}, \mathbf{U}', t) d\xi_j}$$

- $U'_i$ : Lagrangian velocity fluctuation related to the Eulerian mean velocity  $\langle u_i \rangle$ .
- $a_i$  is estimated according to the well-mixed conditions<sup>1</sup>.
- $b_{ij}$  is defined from the Kolmogorov's hypotheses of self-similarity and local isotropy in the inertial subrange<sup>2</sup>.
- $d\xi_j$  incremental Wiener process with zero mean and variance  $dt$ .

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<sup>1</sup>D.J. Thomson, 1987. J. Fluid Mech. **210**, 529-556.

<sup>2</sup>S.B. Pope, 1987. Phys. Fluids **30**, 2374-2379.

# Micromixing model

Molecular diffusivity is simulated by an Interaction by Exchange with the Conditional Mean (IECM) model.

$$\frac{dC}{dt} = -\frac{C - \langle C|u_i \rangle}{\tau_m}$$

- $C$  is the concentration associated to a fluid particle and  $\langle C|u_i \rangle$  is the mean scalar concentration conditioned on the local position and velocity.
- The micromixing time  $\tau_m$  represents the temporal scale of the molecular diffusion:
  - parametrization of  $\tau_m$  follows the formulation of Cassiani et al. (2005a)<sup>3</sup>;
  - $\tau_m$  is assumed to be proportional to the time scale of the relative dispersion process,  $\tau_m = \mu_t \tau_r$ ;
  - $\tau_m = f(\sigma_u, \varepsilon, \sigma_0, t)$

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<sup>3</sup>M. Cassiani, P. Franzese, U. Giostra, 2005a. Atmos. Environ. **39**, 1457-1469.

# SLAM: computational algorithm

## 1. Pre-processing ( $X$ and $U$ ):

- simulation of the trajectories of an ensemble of particles released at the source location;
- estimate of the conditional mean concentration  $\langle C|u_i \rangle$  and the micromixing time  $\tau_m$ .

## 2. Simulation of the concentration fluctuations ( $X, U, C$ ):

- instantaneous release of a uniform particle distribution in the domain;
- initialization of the particle properties ( $X, U, C$ );
- main time loop:
  - loop on all the particles:
    - update particle velocity and position;
    - apply boundary conditions;
    - update particle concentration;
  - update cell-centred statistics;
- update time-averaged statistics.

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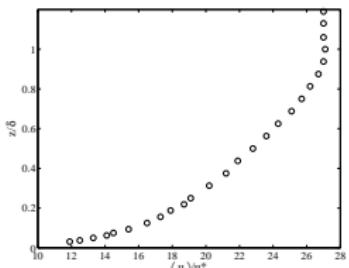
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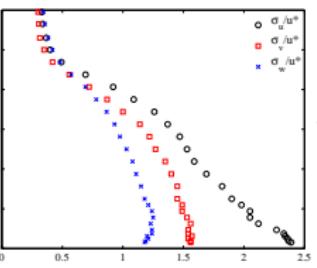
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# Experimental set-up

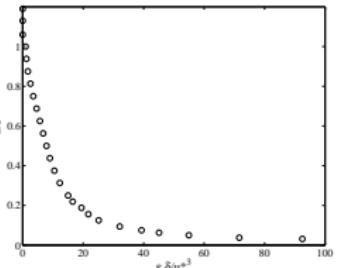
Velocity field → Hot Wire Anemometry measures.



$$1) \frac{\langle u \rangle}{u^*} \text{ vs } \frac{z}{\delta}$$



$$2) \frac{\sigma_u}{u^*}, \frac{\sigma_v}{u^*}, \frac{\sigma_w}{u^*} \text{ vs } \frac{z}{\delta}$$



$$3) \frac{\varepsilon \delta}{u^*^3} \text{ vs } \frac{z}{\delta}$$

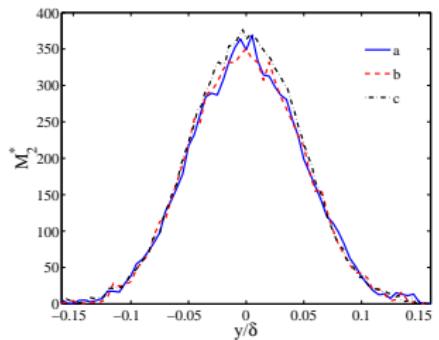
- Boundary layer depth  $\delta = 0.8$  m.
- Friction velocity:  $u^* = 0.185$  m/s.
- Source height  $\frac{h_s}{\delta} = 0.19$ .
- Two source diameters:  $\frac{\phi_1}{\delta} = 3.75\text{e-}3$ ,  $\frac{\phi_2}{\delta} = 7.5\text{e-}3$ .

Concentration field → measures of ethane (passive scalar) concentration by means of Flame Ionization Detector.

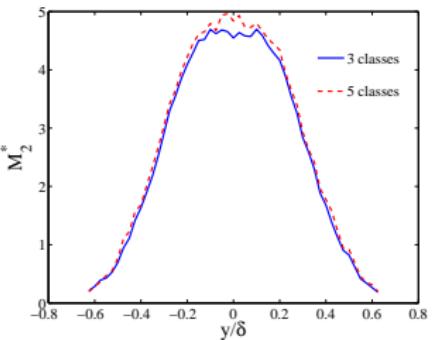
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# Numerical discretization parameters

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1)  $x/\delta = 0.625$



2)  $x/\delta = 5$

Figure:  $M_2^*$  vs  $y/\delta$

- **a:**  $\Delta t = 1e-3$ ,  $\Delta x = 0.02$ ,  $\Delta y = \Delta z = 5e-3$ ;
- **b:**  $\Delta t = 5e-4$ ,  $\Delta x = 0.02$ ,  $\Delta y = \Delta z = 5e-3$ ;
- **c:**  $\Delta t = 1e-3$ ,  $\Delta x = 0.01$ ,  $\Delta y = \Delta z = 3e-3$ .

# Computational set-up

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<b>C<sub>0</sub></b>	<b>σ<sub>0</sub></b>	<b>C<sub>r</sub></b>	<b>μ<sub>t</sub></b>	<b>velocity classes</b>
5.0	$\sqrt{2/3}d_s$	0.3	0.6	$3 \times 3 \times 3$

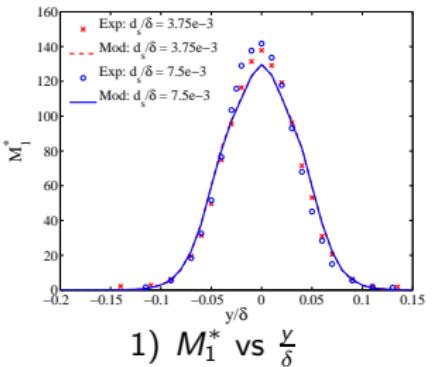
Table: Free parameter values adopted in the simulations

Non-dimensional concentration centred moments:

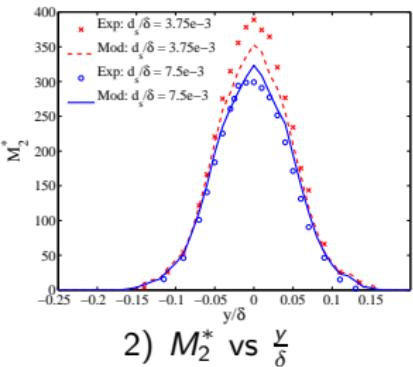
$$M_i^* = \left[ \frac{1}{N_c} \sum_{p=1}^{N_c} (C_p - C_c)^i \right]^{1/i} \frac{u_\infty \delta^2}{Q} \quad i = 1, 2, 3, 4$$

- $u_\infty$ : the velocity at the boundary layer height;
- $N_c$ : number of particles in a discrete volume;
- $C_c$ : mean concentration in a discrete volume;
- $C_p$ : concentration associated to a particle.

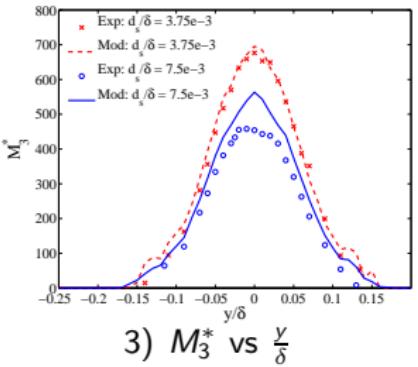
# Results: $M_i^*$ vs $y/\delta$ evaluated at the source height and $x/\delta = 0.625$



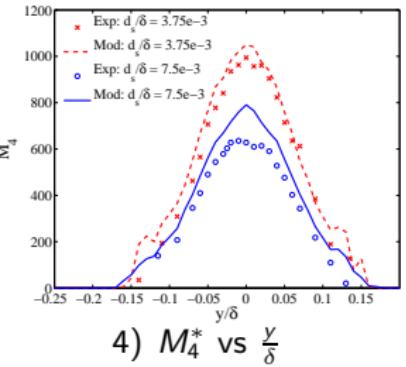
1)  $M_1^* \text{ vs } \frac{y}{\delta}$



2)  $M_2^* \text{ vs } \frac{y}{\delta}$



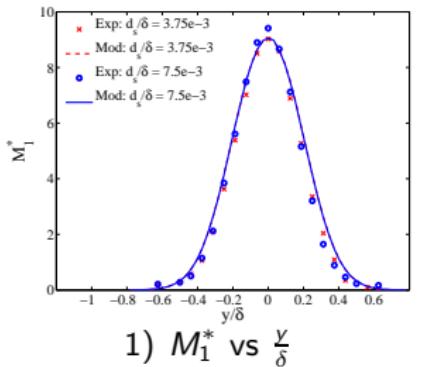
3)  $M_3^* \text{ vs } \frac{y}{\delta}$



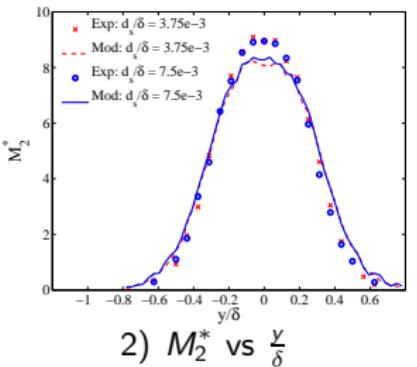
4)  $M_4^* \text{ vs } \frac{y}{\delta}$

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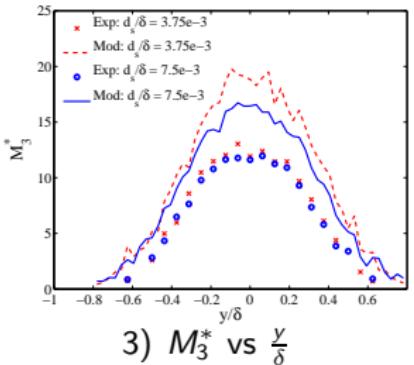
# Results: $M_i^*$ vs $y/\delta$ evaluated at the source height and $x/\delta = 3.75$



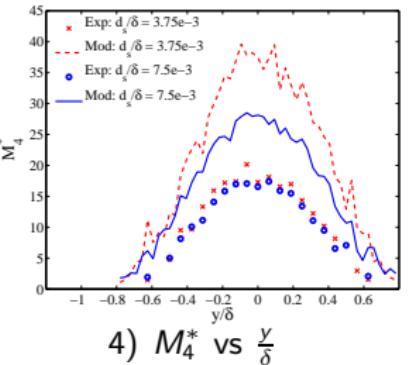
1)  $M_1^* \text{ vs } \frac{y}{\delta}$



2)  $M_2^* \text{ vs } \frac{y}{\delta}$



3)  $M_3^* \text{ vs } \frac{y}{\delta}$



4)  $M_4^* \text{ vs } \frac{y}{\delta}$

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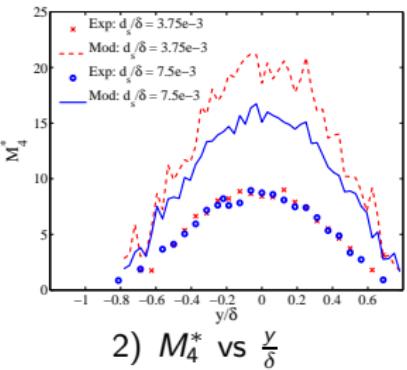
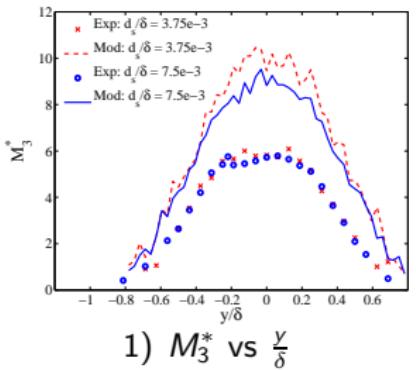
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# Results: $M_i^*$ vs $y/\delta$ evaluated at the source height and $x/\delta = 5.0$



$$D_{rel} = \sqrt{\frac{\int_{-\infty}^{\infty} [(M_i^*)_{S1} - (M_i^*)_{S2}]^2 dy}{\int_{-\infty}^{\infty} [(M_i^*)_{S2}]^2 dy}}$$

$x/\delta$	$D_{rel} M_3^*$	$D_{rel} M_4^*$
3.75	0.17	0.36
5.0	0.12	0.29

Table: Relative difference of the third and fourth moments.

# Conclusions

- The ability of the Lagrangian Stochastic Micromixing model SLAM to estimate concentration fluctuations was investigated.
- The dispersion of a fluctuating plume produced by a continuous release from a point source in a neutral boundary layer was simulated and a comparison with a new experimental data set was performed.
- Good agreement of the first four moments of the concentration close to the source.
- Good agreement of the mean concentration and variance in the far-field.
- Some discrepancies in the third and fourth moments of the concentration in the far-field.

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Thank you for your attention!  
Any questions?